





ภาคผนวก ก.
โปรแกรมจำลอง

มหาวิทยาลัยพระนคร

ลำดับสัญลักษณ์ในโปรแกรม

สัญลักษณ์	ความหมาย	หน่วย
T _{am}	= อุณหภูมิอากาศ	°C
T _{am_K}	= อุณหภูมิอากาศ	K
T _G	= อุณหภูมิกระจก	K
G	= ความเร่งเนื่องจากแรงโน้มถ่วงของโลก	m/s ²
N	= จำนวนเทอร์โม ไซฟอน	-
L _e	= ความยาวส่วนทำระเหยของเทอร์โม ไซฟอน	m
W	= ความกว้างของแผงรับรังสีแสงอาทิตย์	m
A	= พื้นที่รับแสงของแผงรับรังสีแสงอาทิตย์	m ²
K _{air}	= สัมประสิทธิ์การนำความร้อนของอากาศ	W/m.K
Pr	= เลขพริ้นด์เทิลของอากาศ	-
v _{air}	= ปริมาตรจำเพาะของอากาศ	m ³ /s
Emission _{air_1}	= ค่าเปล่งรังสีของกระจก	-
Emission _{air_2}	= ค่าเปล่งรังสีของแผ่นดูดซับรังสี	-
Botmann	= เลขสเตฟาน-โบลมันน์	-
Bate	= สัมประสิทธิ์การขยายตัวเนื่องจากความร้อนเชิงปริมาตร	-
Num	= เลขนิสเซลท์ของอากาศ	-
h _{conv}	= สัมประสิทธิ์การพาความร้อนของอากาศ	W/K
h _{rad}	= สัมประสิทธิ์การแผ่รังสีความร้อนของอากาศ	W/K
z _{conv}	= ความต้านทานความร้อนจากการพาความร้อน	K/W
z _{rad}	= ความต้านทานความร้อนจากการแผ่รังสีความร้อน	K/W
Q _{loss}	= อัตราความร้อนสูญเสียที่แผงรับรังสีแสงอาทิตย์	W
T _{abs_K}	= อุณหภูมิแผ่นดูดซับรังสี	K
T _w	= อุณหภูมิน้ำในถังเก็บ	°C
T _{water}	= อุณหภูมิน้ำในถังเก็บ	K
T _{cond}	= อุณหภูมิที่ส่วนควบแน่นของเทอร์โม ไซฟอน	K
d _{out}	= ขนาดเส้นผ่านศูนย์กลางภายนอกของเทอร์โม ไซฟอน	m
d _{in}	= ขนาดเส้นผ่านศูนย์กลางภายในของเทอร์โม ไซฟอน	m

ลำดับสัญลักษณ์ในโปรแกรม (ต่อ)

สัญลักษณ์	ความหมาย	หน่วย
r_out	= ขนาดรัศมีภายนอกของเทอร์โมไซฟอน	m
r_in	= ขนาดรัศมีภายในของเทอร์โมไซฟอน	m
L_c	= ความยาวส่วนควมแน่นของเทอร์โมไซฟอน	m
L_a	= ความยาวส่วนที่ไม่มีถ่ายเทความร้อน	m
k_cu	= สัมประสิทธิ์การนำความร้อนของเทอร์โมไซฟอน	W/m.K
Specific_Volume	= ปริมาตรจำเพาะของน้ำ	m ³ /kg
Enthalpy_water	= เอนทาลปีของน้ำ	kJ/kg
Thermal_water	= สัมประสิทธิ์การนำความร้อนของน้ำ	W/m.K
Pr_water	= เลขพริ้นด์เทิลของน้ำ	-
Specific_Heat	= ความร้อนจำเพาะของน้ำ	kJ/(kg.K)
Bate_water	= สัมประสิทธิ์การขยายตัวเนื่องจากความร้อนเชิงปริมาตร	-
Ray_water	= เลขเรย์ลีของน้ำ	-
h_cond	= สัมประสิทธิ์การนำความร้อนของน้ำ	W/K
S_co	= พื้นที่ผิวรอบทรงกระบอกในส่วนควมแน่น	m ²
Z ₉	= ค่าความต้านทานความร้อน โดยการพาระหว่างผิวของส่วนควมแน่นกับแหล่งระบายความร้อน	K/W
Q_TS	= อัตราการถ่ายเทความร้อนของเทอร์โมไซฟอน	W
Pressure	= ค่าความดันของสารทำงาน	Pa
Volume_gas	= ปริมาตรจำเพาะของสารทำงาน	m ³ /kg
Enthalpy_134a	= ค่าเอนทาลปีของสารทำงาน	kJ/kg
Thermal_134a	= สัมประสิทธิ์การนำความร้อนของสารทำงาน	W/m.K
cp_134a	= ความร้อนจำเพาะของสารทำงาน	kJ/(kg.K)
Rho_134a	= ค่าความหนาแน่นของสารทำงาน	kg/m ³
Pa	= ค่าความดันบรรยากาศ	Pa
Free2	= merit number	kg/(K ^{0.75} s ^{2.5})
F	= อัตราการเค็มสารทำงาน	%

ลำดับสัญลักษณ์โปรแกรม (ต่อ)

สัญลักษณ์	ความหมาย	หน่วย
Z_2	= ค่าความต้านทานความร้อน โดยการนำผ่านความหนาของผนังท่อเทอร์โมไซฟอน ในส่วนทำระเหย	K/W
Z_8	= ค่าความต้านทานความร้อน โดยการนำ ผ่านความหนาของผนังท่อเทอร์โมไซฟอน ในส่วนควบแน่น	K/W
Z_3f	= ค่าความต้านทานความร้อนฟิล์มของเหลว	K/W
Z_3p	= ค่าความต้านทานความร้อนในแอ่งเดือด	K/W
Z_3	= ค่าความต้านทานความร้อนภายในของของไหลที่กำลังเดือดในเทอร์โมไซฟอน	K/W
Re	= เลขเรย์โนลด์ของสารทำงาน	-
Z_7	= ค่าความต้านทานความร้อนภายในของของไหลที่กำลังควบแน่นในท่อเทอร์โมไซฟอน	K/W
Z_8	= ค่าความต้านทานความร้อน โดยการนำผ่านความหนาของผนังท่อเทอร์โมไซฟอน ในส่วนควบแน่น	K/W
Z_10	= ค่าความต้านทานความร้อนในแนวแกนตามผนังท่อ	K/W
Z_tot	= ค่าความต้านทานความร้อนรวมภายในเทอร์โมไซฟอน	K/W
T_cond_new	= อุณหภูมิที่ส่วนควบแน่นค่าใหม่	K
D_out	= ขนาดเส้นผ่านศูนย์กลางภายนอกของถัง	m
D_in	= ขนาดเส้นผ่านศูนย์กลางภายในของถัง	m
K_fiber	= สัมประสิทธิ์การนำความร้อนของฉนวนกันความร้อน	W/m.K
r_tank_out	= รัศมีภายนอกของถัง	m
r_tank_in	= รัศมีภายในของถัง	m
h_air	= สัมประสิทธิ์การพาความร้อนของอากาศ	W/m.K
Thermal_Al	= สัมประสิทธิ์การนำความร้อนของถัง	W/m.K
Thickness_tank	= ความหนาของถัง	m
Thickness_insulate	= ความหนาของฉนวน	m
Volume_tank	= ปริมาตรในถัง	m ³
m_water	= มวลของน้ำในถัง	kg

ลำดับสัญลักษณ์ในโปรแกรม (ต่อ)

สัญลักษณ์	ความหมาย	หน่วย
Q_{loss}	= อัตราความร้อนสูญเสียที่ถัง	W
Q_{st}	= ความร้อนสะสมของน้ำในถังเก็บ	W
T_{water_new}	= อุณหภูมิของน้ำร้อนในถังเก็บล่าสุด	K



โปรแกรมจำลอง

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Tam1 = 28.25;
Tam2 = 29.45;
Tam3 = 30.51;
Tam4 = 31.56;
Tam5 = 32.81;
Tam6 = 34.10;
Tam7 = 35.21;
Tam8 = 36.15;
Tam9 = 37.08;
Tam10 = 38.08;
Tam11 = 38.95;
Tam12 = 39.15;
Tam13 = 38.81;
Tam14 = 38.15;
Tam15 = 37.23;
Tam16 = 36.33;
Tam17 = 35.43;
Tam18 = 34.6;
Tam19 = 33.73;
Tam20 = 32.68;
Tam21 = 31.68;
Tam22 = 30.78;
Tamtot=
[Tam1, Tam2, Tam3, Tam4, Tam5, Tam6, Tam7, Tam8, Tam9, Tam10, Tam11, Tam12, Tam13, Tam14, Tam15, Tam16, Tam17, Tam18, Tam19, Tam20, Tam21, Tam22];

I1 = 116.8416;
I2 = 204.0354;
I3 = 291.0552;
I4 = 371.8354;
I5 = 466.5760;
I6 = 535.4864;
I7 = 589.2604;
I8 = 679.1093;
I9 = 761.5895;
I10 = 812.1489;
I11 = 840.8229;
I12 = 845.1770;
I13 = 817.9072;
I14 = 772.8010;
I15 = 721.5239;
I16 = 658.9125;
I17 = 593.3000;
I18 = 484.1343;
I19 = 348.8260;
I20 = 251.6479;
I21 = 161.4208;
I22 = 76.1000;

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Itot=
[I1,I2,I3,I4,I5,I6,I7,I8,I9,I10,I11,I12,I13,I14,I15,I16,I17,I18,I19,I20
,I21,I22];
N=10;
N=20;
N = input('ระบุจำนวนข้อ:');
T_w = input('T_w:');
for num = 0:1:21
num = num + 1;
Itot=[ I1 I2 I3 I4 I5 I6 I7 I8 I9 I10 I11 I12 I13 I14 I15 I16 I17 I18
I19 I20 I21 I22];
Tamtot=[ Tam1 Tam2 Tam3 Tam4 Tam5 Tam6 Tam7 Tam8 Tam9 Tam10 Tam11 Tam12
Tam13 Tam14 Tam15 Tam16 Tam17 Tam18 Tam19 Tam20 Tam21 Tam22];
ro= [1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21 22];
I= interp1(ro, Itot, num);
Tam= interp1(ro, Tamtot, num);
aa34main
end
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"air_1"
Tam_K=Tam+273;
TG=Tam_K+0.5;
% (3) (4) (5)
G=9.81;
% (6) (7)
N=input('N=');
L_e=2;
W=1;
% (8) (9)
A=L_e*W;
% (10)
"Input data air_1"
Tav_air_1=(TG-(0.25*(TG-Tam_K)));
T_air_1 = [ 100      150      200      250      300
350      400      450      500      550      600      650
700      750      800      850      900 ];
Pr_air_1 = [ 0.7860  0.7580  0.7370  0.7200  0.7070
0.7000  0.6900  0.6860  0.6840  0.6830  0.6850  0.6900
0.6950  0.7020  0.7090  0.7160  0.7200 ];
Thermal_cond_air_1 = [ 9.34  13.8  18.1  22.3  26.3
30  33.8  37.3  40.7  43.9  46.9  49.7
52.4  54.9  57.3  59.6  62.0 ];
Kinematic_air_1 = [ 2  4.4426  7.59  11.44  15.89
20.92  26.41  32.39  38.79  45.57  52.69  60.21
68.1  76.37  84.93  93.80  102.90 ];
% (11) (12) (13) (14) (15)
% (16) (17) (18)
K_air_1 = interp1 (T_air_1, Thermal_cond_air_1, Tav_air_1)*10^-3;
Pr_1 = interp1 (T_air_1, Pr_air_1, Tav_air_1);
v_air_1 = interp1 (T_air_1, Kinematic_air_1, Tav_air_1)*10^-6;
Emission_air_1=0.88;
% (19) (20) (21)
Emission_air_2=0.044;
Botmann=5.67*10^-8;
Bate_1=1/(Tam_K+(0.25*(TG-Tam_K)));
GrcPr_1=exp(3.848+(29.146*cos((73.6*pi)/180)));
GrL_1=G* Bate_1*L_e^3*(TG-Tam_K)/( v_air_1^2);
Num_1=0.14*(((GrL_1*Pr_1)^(1/3))-
(GrcPr_1^(1/3)))+0.56*(((GrcPr_1*cos((73.6*pi)/180))^(1/4)));
h_conv_1=(( Num_1* K_air_1)/L_e);
h_rad_1= Emission_air_1* Botmann*(TG+Tam_K)*(TG^2+Tam_K^2);
z_conv_1=1/( h_conv_1*A);
z_rad_1=1/( h_rad_1*A);
Q_loss_1=( TG-Tam_K)/(((1/z_conv_1)+(1/z_rad_1))^-1);
"air_2"
Tabs_K=TG+1;
Tai_air_2=(Tam_K+TG)/2;
Tav_air_2=(Tabs_K-(0.25*( Tabs_K- Tai_air_2)));
T_air_2 = [ 100      150      200      250      300
350      400      450      500      550      600      650
700      750      800      850      900 ];

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Pr_air_2          = [ 0.7860   0.7580   0.7370   0.7200   0.7070
0.7000   0.6900   0.6860   0.6840   0.6830   0.6850   0.6900
0.6950   0.7020   0.7090   0.7160   0.7200];
Thermal_cond_air_2 = [ 9.34    13.8    18.1    22.3    26.3
30     33.8    37.3    40.7    43.9    46.9    49.7
52.4   54.9   57.3   59.6   62.0 ];
Kinematic_air_2   = [ 2       4.4426  7.59    11.44   15.89
20.92  26.41  32.39  38.79  45.57  52.69  60.21
68.1   76.37  84.93  93.80  102.90];
T_air(K), Rho_air(kg/m^3), Thermal_cond(W/m-K),
Kinematic_air(m^2/s), Alpha_air(Thermal diffusivity: m^2/s),
Viscosity_air(Pa.s),
K_air_2          = interp1 (T_air_2, Thermal_cond_air_2, Tav_air_2)*10^-3;
Pr_2             = interp1 (T_air_2, Pr_air_2, Tav_air_2);
v_air_2         = interp1 (T_air_2, Kinematic_air_2, Tav_air_2)*10^-6;
Bate_2=1/( Tai_air_2+(0.25*( Tabs_K - Tai_air_2)));
GrcPr_2=exp(3.848+(29.146*cos((73.6*pi)/180)));
GrL_2=G* Bate_2*L_e^3*( Tabs_K - Tai_air_2)/( v_air_2^2);
Num_2=0.14*((GrL_2* Pr_2)^(1/3))-
(GrcPr_2^(1/3))+0.56*((GrcPr_2*cos((73.6*3.142)/180))^(1/4));
h_conv_2=(( Num_2* K_air_2)/L_e);
h_rad_2= Emission_air_2* Botmann*( Tabs_K +TG)*( Tabs_K ^2+TG^2);
z_conv_2=1/( h_conv_2*A);
z_rad_2=1/( h_rad_2*A);
Q_loss_2=(Tabs_K -TG)/(((1/z_conv_2)+(1/z_rad_2))^-1);
pal=abs(Q_loss_1-Q_loss_2);
while pal >= 0.05
    Tabs_K_new=Tabs_K+0.005;
    Tai_air_2=(Tam_K+TG)/2;
    Tav_air_2_new=(Tabs_K_new-(0.25*( Tabs_K_new- Tai_air_2)));
    T_air_2          = [ 100    150    200    250    300
350    400    450    500    550    600    650
700    750    800    850    900 ];
    Pr_air_2          = [ 0.7860   0.7580   0.7370   0.7200
0.7070   0.7000   0.6900   0.6860   0.6840   0.6830   0.6850
0.6900   0.6950   0.7020   0.7090   0.7160   0.7200];
    Thermal_cond_air_2 = [ 9.34    13.8    18.1    22.3    26.3
30     33.8    37.3    40.7    43.9    46.9    49.7
52.4   54.9   57.3   59.6   62.0 ];
    Kinematic_air_2   = [ 2       4.4426  7.59    11.44
15.89  20.92  26.41  32.39  38.79  45.57  52.69
60.21  68.1   76.37  84.93  93.80  102.90];
    T_air(K), Rho_air(kg/m^3), Thermal_cond(W/m-K),
Kinematic_air(m^2/s), Alpha_air(Thermal diffusivity: m^2/s),
Viscosity_air(Pa.s),
    K_air_2_new      = interp1 (T_air_2, Thermal_cond_air_2,
Tav_air_2_new)*10^-3;
    Pr_2_new         = interp1 (T_air_2, Pr_air_2, Tav_air_2_new);
    v_air_2_new      = interp1 (T_air_2, Kinematic_air_2,
Tav_air_2_new)*10^-6;
    Bate_2_new=1/( Tai_air_2+(0.25*( Tabs_K_new - Tai_air_2)));
    GrcPr_2_new=exp(3.848+(29.146*cos((73.6*pi)/180)));
    GrL_2_new=G* Bate_2_new*L_e^3*( Tabs_K_new -
Tai_air_2)/( v_air_2_new^2);

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    Num_2_new=0.14*(((GrL_2_new* Pr_2_new)^(1/3))-
    (GrcPr_2_new^(1/3)))+0.56*(((GrcPr_2_new*cos((73.6*3.142)/180))^(1/4));
    h_conv_2_new=(( Num_2_new* K_air_2_new)/L_e);
    h_rad_2_new= Emission_air_2* Botmann*( Tabs_K_new +TG)*( Tabs_K_new
    ^2+TG^2);
    z_conv_2_new=1/( h_conv_2_new*A);
    z_rad_2_new=1/( h_rad_2_new*A);
    Q_loss_2_new=( Tabs_K_new -
    TG)/(((1/z_conv_2_new)+(1/z_rad_2_new))^-1);
    pal=abs(Q_loss_1-Q_loss_2_new);
    Tabs_K=Tabs_K_new;
end
T_w=input('T_w:');
T_water=T_w+273.15;
T_cond=T_water+1;
d_out = 0.02222;
d_in = 0.02108;
r_out = d_out/2;
r_in = d_in/2;
L_c = 0.478726;
L_e = 2;
L_a = 0.055;
k_cu = 398.4;
%Calculate Q_TS_i
Tav_tank=(T_cond+T_water)/2;
T_water_tank = [ 273.15      275      280      285
290      295      300      305      310      315
320      325      330      335      340      345
350      355      360      365      370      373.15
375      380      385      390      400      410
420      430      440      450      460      470
480      490      500      510      520      530
540      550      560      570      580      590
600      610      620      625      630      635
640      645      647.3 ];
Specific_Volume_Liquid = [ 1.000      1.000      1.000      1.000
1.001      1.002      1.003      1.005      1.007      1.009
1.011      1.013      1.016      1.018      1.021      1.024
1.027      1.030      1.034      1.038      1.041      1.044
1.045      1.049      1.053      1.058      1.067      1.077
1.088      1.099      1.110      1.123      1.137      1.152
1.167      1.184      1.203      1.222      1.244      1.268
1.294      1.323      1.355      1.392      1.433      1.482
1.541      1.612      1.705      1.778      1.856      1.935
2.075      2.351      3.170 ];
Specific_Volume_Gas = [ 206.3      181.7      130.4      99.4
69.7      51.94      39.13      29.74      22.93      17.82
13.98      11.06      8.82      7.09      5.74      4.683
3.846      3.180      2.645      2.212      1.861      1.679
1.574      1.337      1.142      0.980      0.731      0.553
0.425      0.331      0.261      0.208      0.167      0.136
0.111      0.0922      0.0766      0.0631      0.0525      0.0445
0.0375      0.0317      0.0269      0.0228      0.0193      0.0163

```

```

0.0137      0.0115      0.0094      0.0085      0.0075      0.0066
0.0057      0.0045      0.0032 ];
Thermal_cond_water = [ 569      574      582      590
598      606      613      620      628      634
640      645      650      656      660      668
668      671      674      677      679      680
681      683      685      686      688      688
688      685      682      678      673      667
660      651      642      631      621      608
594      580      563      548      528      513
497      467      444      430      412      392
367      331      238 ];
Viscosity_Liquid_water = [ 1750      1652      1422      1225
1080      959      855      769      695      631
577      528      489      453      420      389
365      343      324      306      298      279
274      260      248      237      217      200
185      173      162      152      143      136
129      124      118      113      108      104
101      97      94      91      88      84
81      77      72      70      67      64
59      54      45 ];
Pr_Liquid_water = [ 12.99      12.22      10.26      8.81
7.56      6.62      5.83      5.20      4.62      4.16
3.77      3.42      3.15      2.88      2.66      2.45
2.29      2.14      2.02      1.91      1.80      1.76
1.70      1.61      1.53      1.47      1.34      1.24
1.16      1.09      1.04      0.99      0.95      0.92
0.89      0.87      0.86      0.85      0.84      0.85
0.86      0.87      0.90      0.94      0.99      1.05
1.14      1.30      1.52      1.65      2.0      2.7
4.2      12      0 ];
Specific_Heat_Liquid = [ 4.217      4.211      4.198      4.189
4.184      4.181      4.179      4.178      4.178      4.179
4.180      4.182      4.184      4.186      4.188      4.191
4.195      4.199      4.203      4.209      4.214      4.217
4.220      4.226      4.232      4.239      4.256      4.278
4.302      4.331      4.360      4.400      4.440      4.480
4.530      4.590      4.660      4.740      4.840      4.950
5.080      5.240      5.430      5.680      6.000      6.410
7.000      7.850      9.350      10.600      12.600      16.400
26.000      90.000      0.000 ];
Specific_Volume_L = interp1 (T_water_tank, Specific_Volume_Liquid,
Tav_tank)*10^-3;
Specific_Volume_G = interp1 (T_water_tank, Specific_Volume_Gas,
Tav_tank);
Thermal_water = interp1 (T_water_tank, Thermal_cond_water,
Tav_tank)*10^-3;
Viscosity_water = interp1 (T_water_tank, Viscosity_Liquid_water,
Tav_tank)*10^-6;
Pr_water = interp1 (T_water_tank, Pr_Liquid_water, Tav_tank);
Specific_Heat = interp1 (T_water_tank, Specific_Heat_Liquid,
Tav_tank)*10^3;
Rho_water = (1 / Specific_Volume_L);

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```

Kinematic_water = (Viscosity_water / Rho_water);
Thermal_diffus_water = Thermal_water / (Rho_water*Specific_Heat);
Bate_water = 1 / ((T_cond+T_water)/2);
Ray_water = abs(G*Bate_water*(d_out^3)*(T_cond -
T_water))/(Kinematic_water*Thermal_diffus_water);
h_cond = (Thermal_water / d_out)*(0.6 +
((0.387)*(Ray_water^(1/6)))) / (1 + (0.559 /
Pr_water^(9/16))^(8/27))^2;
S_co = pi*d_out*L_c;
S_co=pi*d^2;
Z_9 = 1/(h_cond*S_co);
Q_TS_1=(T_cond-T_water)/Z_9;
Calculate Q_TS_2
Tav_syphon=(T_cond + Tabs_K)/2;
T_134a = [ 273.15      275.15      277.15      279.15
281.15      283.15      285.15      287.15      289.15      291.15
293.15      295.15      297.15      299.15      301.15      303.15
305.15      307.15      309.15      311.15      313.15      315.15
317.15      319.15      321.15      323.15      325.15      327.15
329.15      331.15      333.15      335.15      337.15      339.15
341.15      343.15      345.15      347.15      349.15      351.15
353.15      358.15      363.15      368.15      373.15      374.18 ];
Rho_134a_Liquid = [ 1293.7      1287.1      1280.5      1273.8
1267.0      1260.2      1253.3      1246.3      1239.3      1232.1
1224.9      1217.5      1210.1      1202.6      1194.9      1187.2
1179.3      1171.3      1163.2      1154.9      1146.5      1137.9
1129.2      1120.3      1111.3      1102.0      1092.6      1082.9
1073.0      1062.8      1052.4      1041.7      1030.7      1019.4
1007.7      995.6      983.1      970.0      956.5      942.3
927.4      886.2      836.9      771.6      646.7      513.3 ];
Pressure_134a = [ 0.29269      0.31450      0.33755      0.36186
0.38749      0.41449      0.44289      0.47276      0.50413      0.53706
0.57159      0.60777      0.65466      0.68531      0.72676      0.77008
0.81530      0.86250      0.91172      0.96301      1.0165      1.0721
1.1300      1.1901      1.2527      1.3177      1.3852      1.4553
1.5280      1.6033      1.6815      1.7625      1.8464      1.9334
2.0234      2.1165      2.2130      2.3127      2.4159      2.5227
2.6331      2.9259      3.2445      3.5916      3.9721      4.0560 ];
Volume_134a_gas = [ 0.06935      0.06470      0.06042      0.05648
0.05284      0.04948      0.04636      0.04348      0.04081      0.03833
0.03606      0.03388      0.03189      0.03003      0.02829      0.02667
0.02516      0.02374      0.02241      0.02116      0.01999      0.01890
0.01786      0.01689      0.01598      0.01511      0.01430      0.01353
0.01280      0.01212      0.01146      0.01085      0.01026      0.00970
0.00917      0.00867      0.00818      0.00772      0.00728      0.00686
0.00646      0.00550      0.00461      0.00374      0.00265      0.00195 ];
Enthalpy_134a_Liquid = [ 200.00      202.68      205.37      208.08
210.80      213.53      216.27      219.03      221.80      224.59
227.40      230.21      233.05      235.90      238.77      241.65
244.55      247.47      250.41      253.37      256.35      259.35
262.38      265.42      268.49      271.59      274.71      277.86
281.04      284.25      287.49      290.77      294.08      297.44
300.84      304.29      307.79      311.34      314.96      318.65
322.41      332.27      343.01      355.43      347.02      389.78 ];

```

```

Enthalpy_134a_gas = [ 398.68      399.84      401.00      402.14
403.27      404.40      405.51      406.61      407.70      408.78
409.84      410.89      411.93      412.95      413.95      414.94
415.90      416.85      417.78      418.69      419.85      420.35
421.28      422.09      422.88      423.63      424.35      425.03
425.68      426.29      426.86      427.37      427.84      428.25
428.61      428.89      429.10      429.23      429.27      429.20
429.02      427.91      425.48      420.60      407.08      389.78 ];
Thermal_cond_134a = [ 93.4      92.5      91.6      90.7
89.7      88.8      87.9      87      86      85.1
84.2      83.3      82.4      81.4      80.5      79.6
78.7      77.7      76.8      75.9      75      74.1
73.1      72.2      71.3      70.4      69.5      68.5
67.6      66.7      65.8      64.9      63.9      63
62.1      61.2      60.3      59.3      58.4      57.5
56.6      54.3      0      0      0      0 ];
Viscosity_134a = [ 287.4      280.4      273.6      267.0
260.6      254.3      248.3      242.5      236.8      231.2
225.8      220.5      215.4      210.4      205.5      200.7
196.0      191.4      186.9      182.5      178.2      174.0
169.8      165.7      161.7      157.7      153.8      149.9
146.1      142.3      138.6      134.9      131.2      127.5
123.9      120.3      116.7      113.1      109.4      105.8
102.1      92.7      82.6      70.9      53.0      0 ];
Specific_134a_Liquid = [ 1.335      1.341      1.347      1.353
1.360      1.367      1.374      1.381      1.388      1.396
1.404      1.412      1.420      1.429      1.438      1.447
1.457      1.467      1.478      1.489      1.500      1.513
1.525      1.539      1.553      1.569      1.585      1.602
1.621      1.641      1.663      1.686      1.712      1.740
1.772      1.806      1.846      1.890      1.941      2.000
2.069      2.313      2.766      3.961      0      0 ];
Pr_134a = [ 4.108      4.065      4.023      3.983
3.951      3.915      3.881      3.849      3.882      3.793
3.765      3.738      3.712      3.694      3.671      3.648
3.629      3.614      3.597      3.580      3.564      3.553
3.542      3.532      3.522      3.515      3.508      3.506
3.503      3.501      3.503      3.504      3.515      3.521
3.535      3.550      3.573      3.605      3.636      3.680
3.732      3.949      0      0      0      0 ];
Rho_134a_L = interp1 (T_134a, Rho_134a_Liquid, Tav_syphon);
Pressure = interp1 (T_134a, Pressure_134a, Tav_syphon)*10^6;
Volume_gas = interp1 (T_134a, Volume_134a_gas, Tav_syphon);
Enthalpy_134a_g = interp1 (T_134a, Enthalpy_134a_gas, Tav_syphon)*10^3;
Enthalpy_134a_L = interp1 (T_134a, Enthalpy_134a_Liquid,
Tav_syphon)*10^3;
Thermal_134a = interp1 (T_134a, Thermal_cond_134a, Tav_syphon)*10^-3;
Viscosity = interp1 (T_134a, Viscosity_134a, Tav_syphon)*10^-6;
cp_134a = interp1 (T_134a, Specific_134a_Liquid,
Tav_syphon)*10^3;
Pr = interp1 (T_134a, Pr_134a, Tav_syphon);
Rho_134a_gas = ( 1 / Volume_gas);
Kinematic = (Viscosity / Rho_134a_L);
Volume_134a_Liquid = (1 / Rho_134a_L);

```

```

Enthalpy_Diff      = Enthalpy_134a_g - Enthalpy_134a_L;
% Rho_134a(kg/m^3), V_kma_gas(m^3/kg), Enthalpy_Diff(J/kg),
Pressure(Pa), Thermal_134a(J/kg-K), Viscosity(Pa.s), cp_134a(J/kg-K)
Pa      = 0.10132*10^6;
Free2=((Enthalpy_Diff*(Thermal_134a^3)*(Rho_134a_L^2))/Viscosity)^0.25;
Free3=28.079*((Pressure / Pa)^0.23);
F      = 0.7;
ln(d_out/d_in)=ln(dia
%ln(0.0222/0.02108);%0.05266
ln_dia=0.05266;
Z_2=ln_dia/(2*pi*L_e*k_cu);
Z_8=ln_dia/(2*pi*L_c*k_cu);
Z_3f = (0.235*(Q_TS_1^(1/3))) /
((d_in^(4/3))*(G^(1/3))*L_e*(Free2^(4/3)));
Z_3p = 1/((Free3)*(G^0.2)*(Q_TS_1^0.4)*((pi*d_in*L_e)^0.6));
if Z_3p < Z_3f
    Z_3 = Z_3p;
else
    Z_3 = (Z_3p*F) + (Z_3f*(1 - F));
end
% Calculate Z_7
Re = (4*Q_TS_1)/(Enthalpy_Diff*Viscosity*pi*d_in);
if Re>1300
    Z_7 = (0.235*(Q_TS_1^(1/3))) /
((d_in^(4/3))*(G^(1/3))*L_c*(Free2^(4/3)))*(191*(Re^-0.733));
else
    Z_7 = (0.235*(Q_TS_1^(1/3))) /
((d_in^(4/3))*(G^(1/3))*L_c*(Free2^(4/3)));
end
Z_8 = ln_dia / (2*pi*L_c*k_cu);
% Calculate Z_10
a_across = (pi*((d_out^2)-(d_in^2))) / 4;
Z_10 = ((0.5*L_e) + L_a + (0.5*L_c)) / (a_across*k_cu);
Z_p = Z_10 / (Z_2 + Z_3 + Z_7 + Z_8);
if Z_p > 20
    Z_tot = Z_2 + Z_3 + Z_7 + Z_8;
else
    Z_tot = ((Z_2 + Z_3 + Z_7 + Z_8)^-1 + (1/Z_10))^-1;
end
Q_TS_2=(Tabs_K-T_cond)/Z_tot;
if Q_TS_2<=0
    Q_TS_1_new=Q_TS_1;
else
pa2=abs(Q_TS_1-Q_TS_2);
if pa2 < 20
    Q_TS_1_new=Q_TS_1;
end
while pa2 >20
    T_cond_new=T_cond+0.02;
    calculate Q_TS_1_new
    Tav_tank=(T_cond_new+T_water)/2;
    T_water_tank
290          295          300          305          310          315          340          345
320          325          330          335          340          345          345          345
= [ 273.15      275      280      285

```

350	355	360	365	370	373.15
375	380	385	390	400	410
420	430	440	450	460	470
480	490	500	510	520	530
540	550	560	570	580	590
600	610	620	625	630	635
640	645	647.3];			
Specific_Volume_Liquid = [1.000 1.000 1.000					
1.000	1.001	1.002	1.003	1.005	1.007
1.009	1.011	1.013	1.016	1.018	1.021
1.024	1.027	1.030	1.034	1.038	1.041
1.044	1.045	1.049	1.053	1.058	1.067
1.077	1.088	1.099	1.110	1.123	1.137
1.152	1.167	1.184	1.203	1.222	1.244
1.268	1.294	1.323	1.355	1.392	1.433
1.482	1.541	1.612	1.705	1.778	1.856
1.935	2.075	2.351	3.170];		
Specific_Volume_Gas = [206.3 181.7 130.4					
99.4	69.7	51.94	39.13	29.74	22.93
17.82	13.98	11.06	8.82	7.09	5.74
4.683	3.846	3.180	2.645	2.212	1.861
1.679	1.574	1.337	1.142	0.980	0.731
0.553	0.425	0.331	0.261	0.208	0.167
0.136	0.111	0.0922	0.0766	0.0631	0.0525
0.0445	0.0375	0.0317	0.0269	0.0228	0.0193
0.0163	0.0137	0.0115	0.0094	0.0085	0.0075
0.0066	0.0057	0.0045	0.0032];		
Thermal_cond_water = [569 574 582 590					
598	606	613	620	628	634
640	645	650	656	660	668
668	671	674	677	679	680
681	683	685	686	688	688
688	685	682	678	673	667
660	651	642	631	621	608
594	580	563	548	528	513
497	467	444	430	412	392
367	331	238];			
Viscosity_Liquid_water = [1750 1652 1422 631					
1225	1080	959	855	769	695
577	528	489	453	420	389
365	343	324	306	298	279
274	260	248	237	217	200
185	173	162	152	143	136
129	124	118	113	108	104
101	97	94	91	88	84
81	77	72	70	67	64
59	54	45];			
Pr_Liquid_water = [12.99 12.22 10.26					
8.81	7.56	6.62	5.83	5.20	4.62
4.16	3.77	3.42	3.15	2.88	2.66
2.45	2.29	2.14	2.02	1.91	1.80
1.76	1.70	1.61	1.53	1.47	1.34
1.24	1.16	1.09	1.04	0.99	0.95
0.92	0.89	0.87	0.86	0.85	0.84


```

0.85      0.86      0.87      0.90      0.94      0.99
1.05      1.14      1.30      1.52      1.65      2.0
2.7      4.2      12      0      ];
Specific_Heat_Liquid = [ 4.217      4.211      4.198
4.189      4.184      4.181      4.179      4.178      4.178
4.179      4.180      4.182      4.184      4.186      4.188
4.191      4.195      4.199      4.203      4.209      4.214
4.217      4.220      4.226      4.232      4.239      4.256
4.278      4.302      4.331      4.360      4.400      4.440
4.480      4.530      4.590      4.660      4.740      4.840
4.950      5.080      5.240      5.430      5.680      6.000
6.410      7.000      7.850      9.350      10.600      12.600
16.400      26.000      90.000      0.000 ];
Specific_Volume_L = interp1 (T_water_tank, Specific_Volume_Liquid,
Tav_tank)*10^-3;
Specific_Volume_G = interp1 (T_water_tank, Specific_Volume_Gas,
Tav_tank);
Thermal_water = interp1 (T_water_tank, Thermal_cond_water,
Tav_tank)*10^-3;
Viscosity_water = interp1 (T_water_tank, Viscosity_Liquid_water,
Tav_tank)*10^-6;
Pr_water = interp1 (T_water_tank, Pr_Liquid_water,
Tav_tank);
Specific_Heat = interp1 (T_water_tank, Specific_Heat_Liquid,
Tav_tank)*10^3;
Rho_water = (1 / Specific_Volume_L);
Kinematic_water = (Viscosity_water / Rho_water);
Thermal_diffus_water = Thermal_water / (Rho_water*Specific_Heat);
Bate_water = 1 / ((T_cond_new+T_water)/2);
Ray_water = abs(G*Bate_water*(d_out^3)*(T_cond_new -
T_water))/(Kinematic_water*Thermal_diffus_water);
h_cond = (Thermal_water / d_out)*(0.6 +
((0.387)*(Ray_water^(1/6)))) / (1 + (0.559 /
Pr_water)^(9/16))^(8/27))^2;
S_co = pi*d_out*L_c;
Z_9 = 1/(h_cond*S_co);
Q_TS_1_new=(T_cond_new-T_water)/Z_9;
*calculate W and Z_new
Tav_syphon=(T_cond_new + Tabs_K)/2;
T_134a = [ 273.15      275.15      277.15
279.15      281.15      283.15      285.15      287.15      289.15
291.15      293.15      295.15      297.15      299.15      301.15
303.15      305.15      307.15      309.15      311.15      313.15
315.15      317.15      319.15      321.15      323.15      325.15
327.15      329.15      331.15      333.15      335.15      337.15
339.15      341.15      343.15      345.15      347.15      349.15
351.15      353.15      358.15      363.15      368.15      373.15
374.18 ];
Rho_134a_Liquid = [ 1293.7      1287.1      1280.5
1273.8      1267.0      1260.2      1253.3      1246.3      1239.3
1232.1      1224.9      1217.5      1210.1      1202.6      1194.9
1187.2      1179.3      1171.3      1163.2      1154.9      1146.5
1137.9      1129.2      1120.3      1111.3      1102.0      1092.6

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1082.9    1073.0    1062.8    1052.4    1041.7    1030.7
1019.4    1007.7    995.6     983.1     970.0     956.5
942.3     927.4     886.2     836.9     771.6     646.7
513.3 ];
  Pressure_134a      = [ 0.29269    0.31450    0.33755
0.36186    0.38749    0.41449    0.44289    0.47276    0.50413
0.53706    0.57159    0.60777    0.65466    0.68531    0.72676
0.77008    0.81530    0.86250    0.91172    0.96301    1.0165
1.0721     1.1300     1.1901     1.2527     1.3177     1.3852
1.4553     1.5280     1.6033     1.6815     1.7625     1.8464
1.9334     2.0234     2.1165     2.2130     2.3127     2.4159
2.5227     2.6331     2.9259     3.2445     3.5916     3.9721
4.0560 ];
  Volume_134a_gas    = [ 0.06935    0.06470    0.06042
0.05648    0.05284    0.04948    0.04636    0.04348    0.04081
0.03833    0.03606    0.03388    0.03189    0.03003    0.02829
0.02667    0.02516    0.02374    0.02241    0.02116    0.01999
0.01890    0.01786    0.01689    0.01598    0.01511    0.01430
0.0353     0.01280    0.01212    0.01146    0.01085    0.01026
0.00970    0.00917    0.00867    0.00818    0.00772    0.00728
0.00686    0.00646    0.00550    0.00461    0.00374    0.00265
0.00195 ];
  Enthalpy_134a_Liquid = [ 200.00    202.68    205.37
208.08     210.80    213.53    216.27    219.03    221.80
224.59     227.40    230.21    233.05    235.90    238.77
241.65     244.55    247.47    250.41    253.37    256.35
259.35     262.38    265.42    268.49    271.59    274.71
277.86     281.04    284.25    287.49    290.77    294.08
297.44     300.84    304.29    307.79    311.34    314.96
318.65     322.41    332.27    343.01    355.43    347.02
389.78 ];
  Enthalpy_134a_gas    = [ 398.68    399.84    401.00
402.14     403.27    404.40    405.51    406.61    407.70
408.78     409.84    410.89    411.93    412.95    413.95
414.94     415.90    416.85    417.78    418.69    419.85
420.35     421.28    422.09    422.88    423.63    424.35
425.03     425.68    426.29    426.86    427.37    427.84
428.25     428.61    428.89    429.10    429.23    429.27
429.20     429.02    427.91    425.48    420.60    407.08
389.78 ];
  Thermal_cond_134a   = [ 93.4     92.5     91.6     90.7
89.7     88.8     87.9     87     86     85.1
84.2     83.3     82.4     81.4    80.5    79.6
78.7     77.7     76.8     75.9    75     74.1
73.1     72.2     71.3     70.4    69.5    68.5
67.6     66.7     65.8     64.9    63.9    63
62.1     61.2     60.3     59.3    58.4    57.5
56.6     54.3     0         0         0         0 ];
  Viscosity_134a     = [ 287.4    280.4    273.6    267.0
260.6    254.3    248.3    242.5    236.8    231.2
225.8    220.5    215.4    210.4    205.5    200.7
196.0    191.4    186.9    182.5    178.2    174.0
169.8    165.7    161.7    157.7    153.8    149.9
146.1    142.3    138.6    134.9    131.2    127.5

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```

123.9      120.3      116.7      113.1      109.4      105.8
102.1      92.7       82.6       70.9       53.0       0 ];
Specific_134a_Liquid = [ 1.335      1.341      1.347      1.353
1.360      1.367      1.374      1.381      1.388      1.396
1.404      1.412      1.420      1.429      1.438      1.447
1.457      1.467      1.478      1.489      1.500      1.513
1.525      1.539      1.553      1.569      1.585      1.602
1.621      1.641      1.663      1.686      1.712      1.740
1.772      1.806      1.846      1.890      1.941      2.000
2.069      2.313      2.766      3.961      0          0 ];
Pr_134a    = [ 4.108      4.065      4.023      3.983
3.951      3.915      3.881      3.849      3.882      3.793
3.765      3.738      3.712      3.694      3.671      3.648
3.629      3.614      3.597      3.580      3.564      3.553
3.542      3.532      3.522      3.515      3.508      3.506
3.503      3.501      3.503      3.504      3.515      3.521
3.535      3.550      3.573      3.605      3.636      3.680
3.732      3.949      0          0          0          0 ];
Rho_134a_L = interp1 (T_134a, Rho_134a_Liquid, Tav_syphon);
Pressure    = interp1 (T_134a, Pressure_134a, Tav_syphon)*10^6;
Volume_gas  = interp1 (T_134a, Volume_134a_gas, Tav_syphon);
Enthalpy_134a_g = interp1 (T_134a, Enthalpy_134a_gas,
Tav_syphon)*10^3;
Enthalpy_134a_L = interp1 (T_134a, Enthalpy_134a_Liquid,
Tav_syphon)*10^3;
Thermal_134a = interp1 (T_134a, Thermal_cond_134a,
Tav_syphon)*10^-3;
Viscosity    = interp1 (T_134a, Viscosity_134a, Tav_syphon)*10^-
6;
cp_134a     = interp1 (T_134a, Specific_134a_Liquid,
Tav_syphon)*10^3;
Pr           = interp1 (T_134a, Pr_134a, Tav_syphon);
Rho_134a_gas = ( 1 / Volume_gas);
Kinematic    = (Viscosity / Rho_134a_L);
Volume_134a_Liquid = (1 / Rho_134a_L);
Enthalpy_Diff = Enthalpy_134a_g - Enthalpy_134a_L;
Rho_134a(kg/m^3), Volume_gas(m^3/kg), Enthalpy_134a_g(kJ/kg),
Pressure(Pa), Thermal_134a(K/m-K), Viscosity(Pa.s), cp_134a(J/kg-K)
Pa = 0.10132*10^6;

Free2=((Enthalpy_Diff*(Thermal_134a^3)*(Rho_134a_L^2))/Viscosity)^0.25;
Free3=28.079*((Pressure / Pa)^0.23);
F      = 0.7;
ln(d_out/d_in)=ln_dia
ln(0.0222/0.02108)=0.05266
n_dia=0.05266;
Z_2=ln_dia/(2*pi*L_e*k_cu);
Z_8=ln_dia/(2*pi*L_c*k_cu);
Z_3f = (0.235*(Q_TS_1_new^(1/3))) /
((d_in^(4/3))*(G^(1/3))*L_e*(Free2^(4/3)));
Z_3p = 1/((Free3)*(G^0.2)*(Q_TS_1_new^0.4)*((pi*d_in*L_e)^0.6));
if Z_3p < Z_3f
    Z_3 = Z_3p;
else

```

```

        Z_3 = (Z_3p*F) + (Z_3f*(1 - F));
    end
    % Calculate Q_1
    Re = (4*Q_TS_1_new)/(Enthalpy_Diff*Viscosity*pi*d_in);
    if Re>1300
        Z_7 = (0.235*(Q_TS_1_new^(1/3))) /
        ((d_in^(4/3))*(G^(1/3))*L_c*(Free2^(4/3)))*(191*(Re^-0.733));
    else
        Z_7 = (0.235*(Q_TS_1_new^(1/3))) /
        ((d_in^(4/3))*(G^(1/3))*L_c*(Free2^(4/3)));
    end
    % Calculate Z_10
    a_across = (pi*((d_out^2)-(d_in^2))) / 4;
    Z_10 = ((0.5*L_e) + L_a + (0.5*L_c)) / (a_across*k_cu) ;
    Z_p = Z_10 / (Z_2 + Z_3 + Z_7 + Z_8);
    if Z_p > 20
        Z_tot = Z_2 + Z_3 + Z_7 + Z_8;
    else
        Z_tot = ((Z_2 + Z_3 + Z_7 + Z_8)^-1 + (1/Z_10))^-1;
    end
    Q_TS_2_new=(Tabs_K-T_cond_new)/Z_tot;
    if Q_TS_2_new <= 0
        pa2 = 9;
        Q_TS_1_new = Q_TS_1;
    else
        pa2=abs(Q_TS_1_new-Q_TS_2_new);
        T_cond=T_cond_new;
    end
end
end
% calculate QG_1
%T_inpu ('QG1at Radiation ');
transmissivity=0.79;
absorbitivity=0.97;
QG_1=transmissivity*absorbitivity*I*A;
%calculate QG_2
QG_2=(Q_TS_1_new*N)+Q_loss_1;
pa4=abs(QG_1-QG_2);

while pa4>= 160
    TG_new=TG+0.01;
    TG=TG_new;
    %TG, Pa4, N(4)
    G=9.81;
    %G(m/s^2)
    %N=)input('input:');
    L_e=2;
    W=1;
    %T_g, N(3)
    A=L_e*W;
    %A(m^2)
    %("interpolate air_1"

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Tav_air_1=(TG-(0.25*(TG-Tam_K)));
T_air_1 = [ 100      150      200      250      300
350      400      450      500      550      600      650
700      750      800      850      900 ];
Pr_air_1 = [ 0.7860  0.7580  0.7370  0.7200  0.7070
0.7000  0.6900  0.6860  0.6840  0.6830  0.6850  0.6900
0.6950  0.7020  0.7090  0.7160  0.7200];
Thermal_cond_air_1 = [ 9.34  13.8  18.1  22.3  26.3
30  33.8  37.3  40.7  43.9  46.9  49.7
52.4  54.9  57.3  59.6  62.0 ];
Kinematic_air_1 = [ 2  4.4426  7.59  11.44  15.89
20.92  26.41  32.39  38.79  45.57  52.69  60.21
68.1  76.37  84.93  93.80  102.90];
T_air_1(K), rho_air_1(kg/m^3), Thermal_cond_1(W/m^2K),
Kinematic_air_1(m^2/s), Alpha_air_1(m^2/s), Viscosity_air_1(Pa.s)
K_air_1 = interp1 (T_air_1, Thermal_cond_air_1, Tav_air_1)*10^-3;
Pr_1 = interp1 (T_air_1, Pr_air_1, Tav_air_1);
v_air_1 = interp1 (T_air_1, Kinematic_air_1, Tav_air_1)*10^-6;
Emission_air_1=0.88;
-0.80-0.9- in maaahhh
Emission_air_2=0.044;
Botmann=5.67*10^-8;
Bate_1=1/(Tam_K+(0.25*(TG-Tam_K)));
GrcPr_1=exp(3.848+(29.146*cos((73.6*pi)/180)));
GrL_1=G*Bate_1*L_e^3*(TG-Tam_K)/(v_air_1^2);
Num_1=0.14*((GrL_1*Pr_1)^(1/3))-
(GrcPr_1^(1/3))+0.56*((GrcPr_1*cos((73.6*pi)/180))^(1/4));
h_conv_1=((Num_1*K_air_1)/L_e);
h_rad_1= Emission_air_1* Botmann*(TG+Tam_K)*(TG^2+Tam_K^2);
z_conv_1=1/(h_conv_1*A);
z_rad_1=1/(h_rad_1*A);
Q_loss_1=( TG-Tam_K)/(((1/z_conv_1)+(1/z_rad_1))^-1);
%Tabs=interp('Tabs: ');
Tabs_K=TG+1;
%air_1="air_1 Tabs"
%Face_K=1000+1;
Tai_air_2=(Tam_K+TG)/2;
Tav_air_2=(Tabs_K-(0.25*( Tabs_K- Tai_air_2)));
T_air_2 = [ 100      150      200      250      300
350      400      450      500      550      600      650
700      750      800      850      900 ];
Pr_air_2 = [ 0.7860  0.7580  0.7370  0.7200  0.7070
0.7000  0.6900  0.6860  0.6840  0.6830  0.6850  0.6900
0.6950  0.7020  0.7090  0.7160  0.7200];
Thermal_cond_air_2 = [ 9.34  13.8  18.1  22.3  26.3
30  33.8  37.3  40.7  43.9  46.9  49.7
52.4  54.9  57.3  59.6  62.0 ];
Kinematic_air_2 = [ 2  4.4426  7.59  11.44  15.89
20.92  26.41  32.39  38.79  45.57  52.69  60.21
68.1  76.37  84.93  93.80  102.90];
T2_air_2(K), rho_2air_2(kg/m^3), Thermal_cond_2(W/m^2K),
Kinematic_air_2(m^2/s),Alpha_2air_2(thermal diffusivity)(m^2/s),
Viscosity_2air_2(Pa.s),

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K_air_2      = interp1 (T_air_2, Thermal_cond_air_2, Tav_air_2)*10^-3;
Pr_2        = interp1 (T_air_2, Pr_air_2, Tav_air_2);
v_air_2     = interp1 (T_air_2, Kinematic_air_2, Tav_air_2)*10^-6;
Bate_2=1/( Tai_air_2+(0.25*( Tabs_K - Tai_air_2)));
GrcPr_2=exp(3.848+(29.146*cos((73.6*pi)/180)));
GrL_2=G* Bate_2*L_e^3*( Tabs_K - Tai_air_2)/( v_air_2^2);
Num_2=0.14*(((GrL_2* Pr_2)^(1/3))-
(GrcPr_2^(1/3)))+0.56*(((GrcPr_2*cos((73.6*3.142)/180))^(1/4)));
h_conv_2=(( Num_2* K_air_2)/L_e);
h_rad_2= Emission_air_2* Botmann*( Tabs_K +TG)*( Tabs_K ^2+TG^2);
z_conv_2=1/( h_conv_2*A);
z_rad_2=1/( h_rad_2*A);
Q_loss_2=(Tabs_K -TG)/(((1/z_conv_2)+(1/z_rad_2))^-1);
pal=abs(Q_loss_1-Q_loss_2);
while pal >= 0.05
    Tabs_K_new=Tabs_K+0.005;
    Tai_air_2=(Tam_K+TG)/2;
    Tav_air_2_new=(Tabs_K_new-(0.25*( Tabs_K_new- Tai_air_2)));
    T_air_2      = [ 100      150      200      250      300
350      400      450      500      550      600      650
700      750      800      850      900 ];
    Pr_air_2     = [ 0.7860  0.7580  0.7370  0.7200
0.7070  0.7000  0.6900  0.6860  0.6840  0.6830  0.6850
0.6900  0.6950  0.7020  0.7090  0.7160  0.7200];
    Thermal_cond_air_2 = [ 9.34  13.8  18.1  22.3  26.3
30  33.8  37.3  40.7  43.9  46.9  49.7
52.4  54.9  57.3  59.6  62.0 ];
    Kinematic_air_2   = [ 2  4.4426  7.59  11.44
15.89  20.92  26.41  32.39  38.79  45.57  52.69
60.21  68.1  76.37  84.93  93.80  102.90];
    K_air_2      = interp1 (T_air_2, Thermal_cond_air_2,
Tav_air_2_new)*10^-3;
    Pr_2_new     = interp1 (T_air_2, Pr_air_2, Tav_air_2_new);
    v_air_2_new  = interp1 (T_air_2, Kinematic_air_2,
Tav_air_2_new)*10^-6;
    Bate_2_new=1/( Tai_air_2+(0.25*( Tabs_K_new - Tai_air_2)));
    GrcPr_2_new=exp(3.848+(29.146*cos((73.6*pi)/180)));
    GrL_2_new=G* Bate_2_new*L_e^3*( Tabs_K_new -
Tai_air_2)/( v_air_2_new^2);
    Num_2_new=0.14*(((GrL_2_new* Pr_2_new)^(1/3))-
(GrcPr_2_new^(1/3)))+0.56*(((GrcPr_2_new*cos((73.6*3.142)/180))^(1/4)));
    h_conv_2_new=(( Num_2_new* K_air_2_new)/L_e);
    h_rad_2_new= Emission_air_2* Botmann*( Tabs_K_new +TG)*( Tabs_K_new
^2+TG^2);
    z_conv_2_new=1/( h_conv_2_new*A);
    z_rad_2_new=1/( h_rad_2_new*A);
    Q_loss_2_new=( Tabs_K_new -
TG)/(((1/z_conv_2_new)+(1/z_rad_2_new))^-1);
    pal=abs(Q_loss_1-Q_loss_2_new);
    Tabs_K=Tabs_K_new;
end

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T_w=inp('T_water:');
T_water=T_w+273.15;
T_cond=T_water+1;
Tav_tank=(T_cond+T_water)/2;
T_water_tank = [ 273.15      275      280      285
290      295      300      305      310      315
320      325      330      335      340      345
350      355      360      365      370      373.15
375      380      385      390      400      410
420      430      440      450      460      470
480      490      500      510      520      530
540      550      560      570      580      590
600      610      620      625      630      635
640      645      647.3 ];
Specific_Volume_Liquid = [ 1.000      1.000      1.000      1.000      1.000
1.001      1.002      1.003      1.005      1.007      1.009
1.011      1.013      1.016      1.018      1.021      1.024
1.027      1.030      1.034      1.038      1.041      1.044
1.045      1.049      1.053      1.058      1.067      1.077
1.088      1.099      1.110      1.123      1.137      1.152
1.167      1.184      1.203      1.222      1.244      1.268
1.294      1.323      1.355      1.392      1.433      1.482
1.541      1.612      1.705      1.778      1.856      1.935
2.075      2.351      3.170 ];
Specific_Volume_Gas = [ 206.3      181.7      130.4      99.4
69.7      51.94      39.13      29.74      22.93      17.82
13.98      11.06      8.82      7.09      5.74      4.683
3.846      3.180      2.645      2.212      1.861      1.679
1.574      1.337      1.142      0.980      0.731      0.553
0.425      0.331      0.261      0.208      0.167      0.136
0.111      0.0922      0.0766      0.0631      0.0525      0.0445
0.0375      0.0317      0.0269      0.0228      0.0193      0.0163
0.0137      0.0115      0.0094      0.0085      0.0075      0.0066
0.0057      0.0045      0.0032 ];
Thermal_cond_water = [ 569      574      582      590
598      606      613      620      628      634
640      645      650      656      660      668
668      671      674      677      679      680
681      683      685      686      688      688
688      685      682      678      673      667
660      651      642      631      621      608
594      580      563      548      528      513
497      467      444      430      412      392
367      331      238 ];
Viscosity_Liquid_water = [ 1750      1652      1422      1225
1080      959      855      769      695      631
577      528      489      453      420      389
365      343      324      306      298      279
274      260      248      237      217      200
185      173      162      152      143      136
129      124      118      113      108      104

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101          97          94          91          88          84
81           77          72          70          67          64
59           54          45 ];
Pr_Liquid_water = [ 12.99          12.22          10.26          8.81
7.56          6.62          5.83          5.20          4.62          4.16
3.77          3.42          3.15          2.89          2.66          2.45
2.29          2.14          2.02          1.91          1.80          1.76
1.70          1.61          1.53          1.47          1.34          1.24
1.16          1.09          1.04          0.99          0.95          0.92
0.89          0.87          0.86          0.85          0.84          0.85
0.86          0.87          0.90          0.94          0.99          1.05
1.14          1.30          1.52          1.65          2.0          2.7
4.2           12          0 ];
Specific_Heat_Liquid = [ 4.217          4.211          4.198          4.189
4.184          4.181          4.179          4.178          4.178          4.179
4.180          4.182          4.184          4.186          4.188          4.191
4.195          4.199          4.203          4.209          4.214          4.217
4.220          4.226          4.232          4.239          4.256          4.278
4.302          4.331          4.360          4.400          4.440          4.480
4.530          4.590          4.660          4.740          4.840          4.950
5.080          5.240          5.430          5.680          6.000          6.410
7.000          7.850          9.350          10.600          12.600          16.400
26.000          90.000          0.000 ];
Specific_Volume_L = interpl (T_water_tank, Specific_Volume_Liquid,
Tav_tank)*10^-3;
Specific_Volume_G = interpl (T_water_tank, Specific_Volume_Gas,
Tav_tank);
Thermal_water = interpl (T_water_tank, Thermal_cond_water,
Tav_tank)*10^-3;
Viscosity_water = interpl (T_water_tank, Viscosity_Liquid_water,
Tav_tank)*10^=6;
Pr_water = interpl (T_water_tank, Pr_Liquid_water, Tav_tank);
Specific_Heat = interpl (T_water_tank, Specific_Heat_Liquid,
Tav_tank)*10^3;
Rho_water = (1 / Specific_Volume_L);
Kinematic_water = (Viscosity_water / Rho_water);
Thermal_diffus_water = Thermal_water / (Rho_water*Specific_Heat);
Bate_water = 1 / ((T_cond+T_water)/2);
Ray_water = abs(G*Bate_water*(d_out^3)*(T_cond -
T_water))/(Kinematic_water*Thermal_diffus_water);
h_cond = (Thermal_water / d_out)*(0.6 +
((0.387)*(Ray_water^(1/6))) / (1 + (0.559 /
Pr_water)^(9/16))^(8/27))^2;
S_co = pi*d_out*L_c;
{S_co[m^2]}
Z_9 = 1/(h_cond*S_co);
Q_TS_1=(T_cond-T_water)/Z_9;
calculate Q_TS_2
Tav_syphon=(T_cond + Tabs_K)/2;
T_134a = [ 273.15          275.15          277.15          279.15
281.15          283.15          285.15          287.15          289.15          291.15
293.15          295.15          297.15          299.15          301.15          303.15
305.15          307.15          309.15          311.15          313.15          315.15
317.15          319.15          321.15          323.15          325.15          327.15

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329.15	331.15	333.15	335.15	337.15	339.15
341.15	343.15	345.15	347.15	349.15	351.15
353.15	358.15	363.15	368.15	373.15	374.18];
Rho_134a_Liquid		= [1293.7	1287.1	1280.5	1273.8
1267.0	1260.2	1253.3	1246.3	1239.3	1232.1
1224.9	1217.5	1210.1	1202.6	1194.9	1187.2
1179.3	1171.3	1163.2	1154.9	1146.5	1137.9
1129.2	1120.3	1111.3	1102.0	1092.6	1082.9
1073.0	1062.8	1052.4	1041.7	1030.7	1019.4
1007.7	995.6	983.1	970.0	956.5	942.3
927.4	886.2	836.9	771.6	646.7	513.3];
Pressure_134a		= [0.29269	0.31450	0.33755	0.36186
0.38749	0.41449	0.44289	0.47276	0.50413	0.53706
0.57159	0.60777	0.65466	0.68531	0.72676	0.77008
0.81530	0.86250	0.91172	0.96301	1.0165	1.0721
1.1300	1.1901	1.2527	1.3177	1.3852	1.4553
1.5280	1.6033	1.6815	1.7625	1.8464	1.9334
2.0234	2.1165	2.2130	2.3127	2.4159	2.5227
2.6331	2.9259	3.2445	3.5916	3.9721	4.0560];
Volume_134a_gas		= [0.06935	0.06470	0.06042	0.05648
0.05284	0.04948	0.04636	0.04348	0.04081	0.03833
0.03606	0.03388	0.03189	0.03003	0.02829	0.02667
0.02516	0.02374	0.02241	0.02116	0.01999	0.01890
0.01786	0.01689	0.01598	0.01511	0.01430	0.0353
0.01280	0.01212	0.01146	0.01085	0.01026	0.00970
0.00917	0.00867	0.00818	0.00772	0.00728	0.00686
0.00646	0.00550	0.00461	0.00374	0.00265	0.00195];
Enthalpy_134a_Liquid		= [200.00	202.68	205.37	208.08
210.80	213.53	216.27	219.03	221.80	224.59
227.40	230.21	233.05	235.90	238.77	241.65
244.55	247.47	250.41	253.37	256.35	259.35
262.38	265.42	268.49	271.59	274.71	277.86
281.04	284.25	287.49	290.77	294.08	297.44
300.84	304.29	307.79	311.34	314.96	318.65
322.41	332.27	343.01	355.43	347.02	389.78];
Enthalpy_134a_gas		= [398.68	399.84	401.00	402.14
403.27	404.40	405.51	406.61	407.70	408.78
409.84	410.89	411.93	412.95	413.95	414.94
415.90	416.85	417.78	418.69	419.85	420.35
421.28	422.09	422.88	423.63	424.35	425.03
425.68	426.29	426.86	427.37	427.84	428.25
428.61	428.89	429.10	429.23	429.27	429.20
429.02	427.91	425.48	420.60	407.08	389.78];
Thermal_cond_134a		= [93.4	92.5	91.6	90.7
89.7	88.8	87.9	87	86	85.1
84.2	83.3	82.4	81.4	80.5	79.6
78.7	77.7	76.8	75.9	75	74.1
73.1	72.2	71.3	70.4	69.5	68.5
67.6	66.7	65.8	64.9	63.9	63
62.1	61.2	60.3	59.3	58.4	57.5
56.6	54.3	0	0	0	0];
Viscosity_134a		= [287.4	280.4	273.6	267.0
260.6	254.3	248.3	242.5	236.8	231.2
225.8	220.5	215.4	210.4	205.5	200.7

```

196.0      191.4      186.9      182.5      178.2      174.0
169.8      165.7      161.7      157.7      153.8      149.9
146.1      142.3      138.6      134.9      131.2      127.5
123.9      120.3      116.7      113.1      109.4      105.8
102.1      92.7       82.6       70.9       53.0       0 ];
Specific_134a_Liquid = [ 1.335      1.341      1.347      1.353
1.360      1.367      1.374      1.381      1.388      1.396
1.404      1.412      1.420      1.429      1.438      1.447
1.457      1.467      1.478      1.489      1.500      1.513
1.525      1.539      1.553      1.569      1.585      1.602
1.621      1.641      1.663      1.686      1.712      1.740
1.772      1.806      1.846      1.890      1.941      2.000
2.069      2.313      2.766      3.961      0          0 ];
Pr_134a     = [ 4.108      4.065      4.023      3.983
3.951      3.915      3.881      3.849      3.882      3.793
3.765      3.738      3.712      3.694      3.671      3.648
3.629      3.614      3.597      3.580      3.564      3.553
3.542      3.532      3.522      3.515      3.508      3.506
3.503      3.501      3.503      3.504      3.515      3.521
3.535      3.550      3.573      3.605      3.636      3.680
3.732      3.949      0          0          0          0 ];
Rho_134a_L   = interp1 (T_134a, Rho_134a_Liquid, Tav_syphon);
Pressure     = interp1 (T_134a, Pressure_134a, Tav_syphon)*10^6;
Volume_gas   = interp1 (T_134a, Volume_134a_gas, Tav_syphon);
Enthalpy_134a_g= interp1 (T_134a, Enthalpy_134a_gas, Tav_syphon)*10^3;
Enthalpy_134a_L= interp1 (T_134a, Enthalpy_134a_Liquid,
Tav_syphon)*10^3;
Thermal_134a = interp1 (T_134a, Thermal_cond_134a, Tav_syphon)*10^-3;
Viscosity    = interp1 (T_134a, Viscosity_134a, Tav_syphon)*10^-6;
cp_134a     = interp1 (T_134a, Specific_134a_Liquid,
Tav_syphon)*10^3;
Pr           = interp1 (T_134a, Pr_134a, Tav_syphon);
Rho_134a_gas = ( 1 / Volume_gas);
Kinematic    = (Viscosity / Rho_134a_L);
Volume_134a_Liquid = (1 / Rho_134a_L);
Enthalpy_Diff = Enthalpy_134a_g - Enthalpy_134a_L;
rho_134a(kg/m^3), volume_gas(m^3/kg), enthalpy_diff(J/kg),
Pressure(Pa), Thermal_134a(W/m^2K), Viscosity(Pa.s), cp_134a(J/kg-K)
Pa         = 0.10132*10^6;
Free2=((Enthalpy_Diff*(Thermal_134a^3)*(Rho_134a_L^2))/Viscosity)^0.25;
Free3=28.079*((Pressure / Pa)^0.23);
F         = 0.7;
ln(d_out/d_in)=ln_dia
ln((1+2222/9.8210^2)=0.05266
ln_dia=0.05266;
Z_2=ln_dia/(2*pi*L_e*k_cu);
Z_8=ln_dia/(2*pi*L_c*k_cu);
Z_3f = (0.235*(Q_TS_1^(1/3))) /
((d_in^(4/3))*(G^(1/3))*L_e*(Free2^(4/3)));
Z_3p = 1/((Free3)*(G^0.2)*(Q_TS_1^0.4)*((pi*d_in*L_e)^0.6));
if Z_3p < Z_3f
    Z_3 = Z_3p;
else
    Z_3 = (Z_3p*F) + (Z_3f*(1 - F));

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```

end
% Calculate Z_7
Re = (4*Q_TS_1)/(Enthalpy_Diff*Viscosity*pi*d_in);
if Re>1300
    Z_7 = (0.235*(Q_TS_1^(1/3))) /
    ((d_in^(4/3))*(G^(1/3))*L_c*(Free2^(4/3)))*(191*(Re^-0.733));
else
    Z_7 = (0.235*(Q_TS_1^(1/3))) /
    ((d_in^(4/3))*(G^(1/3))*L_c*(Free2^(4/3)));
end
% Calculate Z_10
a_across = (pi*((d_out^2)-(d_in^2))) / 4;
Z_10 = ((0.5*L_e) + L_a + (0.5*L_c)) / (a_across*k_cu) ;
Z_p = Z_10 / (Z_2 + Z_3 + Z_7 + Z_8);
if Z_p > 20
    Z_tot = Z_2 + Z_3 + Z_7 + Z_8;
else
    Z_tot = ((Z_2 + Z_3 + Z_7 + Z_8)^-1 + (1/Z_10))^-1;
end
Q_TS_2=(Tabs_K-T_cond)/Z_tot;
if Q_TS_2<= 0
    Q_TS_1_new = Q_TS_1;
else
    pa2=abs(Q_TS_1-Q_TS_2);
    if pa2 < 20
        Q_TS_1_new=Q_TS_1;
    end
while pa2 >= 20
    T_cond_new=T_cond+0.1;
    % calculate Q_TS_1_new
    Tav_tank=(T_cond_new+T_water)/2;
    T_water_tank = [ 273.15      275      280      285
290      295      300      305      310      315
320      325      330      335      340      345
350      355      360      365      370      373.15
375      380      385      390      400      410
420      430      440      450      460      470
480      490      500      510      520      530
540      550      560      570      580      590
600      610      620      625      630      635
640      645      647.3 ];
    Specific_Volume_Liquid = [ 1.000      1.000      1.000
1.000      1.001      1.002      1.003      1.005      1.007
1.009      1.011      1.013      1.016      1.018      1.021
1.024      1.027      1.030      1.034      1.038      1.041
1.044      1.045      1.049      1.053      1.058      1.067
1.077      1.088      1.099      1.110      1.123      1.137
1.152      1.167      1.184      1.203      1.222      1.244
1.268      1.294      1.323      1.355      1.392      1.433
1.482      1.541      1.612      1.705      1.778      1.856
1.935      2.075      2.351      3.170 ];
    Specific_Volume_Gas = [ 206.3      181.7      130.4
99.4      69.7      51.94      39.13      29.74      22.93
17.82      13.98      11.06      8.82      7.09      5.74

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4.683      3.846      3.180      2.645      2.212      1.861
1.679      1.574      1.337      1.142      0.980      0.731
0.553      0.425      0.331      0.261      0.208      0.167
0.136      0.111      0.0922     0.0766     0.0631     0.0525
0.0445     0.0375     0.0317     0.0269     0.0228     0.0193
0.0163     0.0137     0.0115     0.0094     0.0085     0.0075
0.0066     0.0057     0.0045     0.0032     ];
Thermal_cond_water = [ 569      574      582      590
598      606      613      620      628      634
640      645      650      656      660      668
668      671      674      677      679      680
681      683      685      686      688      688
688      685      682      678      673      667
660      651      642      631      621      608
594      580      563      548      528      513
497      467      444      430      412      392
367      331      238 ];
Viscosity_Liquid_water = [ 1750      1652      1422
1225      1080      959      855      769      695      631
577      528      489      453      420      389
365      343      324      306      298      279
274      260      248      237      217      200
185      173      162      152      143      136
129      124      118      113      108      104
101      97      94      91      88      84
81      77      72      70      67      64
59      54      45 ];
Pr_Liquid_water = [ 12.99      12.22      10.26
8.81      7.56      6.62      5.83      5.20      4.62
4.16      3.77      3.42      3.15      2.88      2.66
2.45      2.29      2.14      2.02      1.91      1.80
1.76      1.70      1.61      1.53      1.47      1.34
1.24      1.16      1.09      1.04      0.99      0.95
0.92      0.89      0.87      0.86      0.85      0.84
0.85      0.86      0.87      0.90      0.94      0.99
1.05      1.14      1.30      1.52      1.65      2.0
2.7      4.2      12      0 ];
Specific_Heat_Liquid = [ 4.217      4.211      4.198
4.189      4.184      4.181      4.179      4.178      4.178
4.179      4.180      4.182      4.184      4.186      4.188
4.191      4.195      4.199      4.203      4.209      4.214
4.217      4.220      4.226      4.232      4.239      4.256
4.278      4.302      4.331      4.360      4.400      4.440
4.480      4.530      4.590      4.660      4.740      4.840
4.950      5.080      5.240      5.430      5.680      6.000
6.410      7.000      7.850      9.350      10.600      12.600
16.400     26.000     90.000     0.000 ];
Specific_Volume_L = interp1 (T_water_tank, Specific_Volume_Liquid,
Tav_tank)*10^-3;
Specific_Volume_G = interp1 (T_water_tank, Specific_Volume_Gas,
Tav_tank);
Thermal_water = interp1 (T_water_tank, Thermal_cond_water,
Tav_tank)*10^-3;

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    Viscosity_water = interp1 (T_water_tank, Viscosity_Liquid_water,
Tav_tank)*10^-6;
    Pr_water = interp1 (T_water_tank, Pr_Liquid_water,
Tav_tank);
    Specific_Heat = interp1 (T_water_tank, Specific_Heat_Liquid,
Tav_tank)*10^3;
    Rho_water = (1 / Specific_Volume_L);
    Kinematic_water = (Viscosity_water / Rho_water);
    Thermal_diffus_water = Thermal_water / (Rho_water*Specific_Heat);
    Bate_water = 1 / ((T_cond_new+T_water)/2);
    Ray_water = abs(G*Bate_water*(d_out^3)*(T_cond_new -
T_water))/(Kinematic_water*Thermal_diffus_water);
    h_cond = (Thermal_water / d_out)*(0.6 +
((0.387)*(Ray_water^(1/6)))) / (1 + (0.559 /
Pr_water)^(9/16))^(8/27))^2;
    S_co = pi*d_out*L_c;
    Z_9 = 1/(h_cond*S_co);
    Q_TS_1_new=(T_cond_new-T_water)/Z_9;
    Tav_syphon=(T_cond_new + Tabs_K)/2;
    T_134a = [ 273.15      275.15      277.15
279.15      281.15      283.15      285.15      287.15      289.15
291.15      293.15      295.15      297.15      299.15      301.15
303.15      305.15      307.15      309.15      311.15      313.15
315.15      317.15      319.15      321.15      323.15      325.15
327.15      329.15      331.15      333.15      335.15      337.15
339.15      341.15      343.15      345.15      347.15      349.15
351.15      353.15      358.15      363.15      368.15      373.15
374.18 ];
    Rho_134a_Liquid = [ 1293.7      1287.1      1280.5
1273.8      1267.0      1260.2      1253.3      1246.3      1239.3
1232.1      1224.9      1217.5      1210.1      1202.6      1194.9
1187.2      1179.3      1171.3      1163.2      1154.9      1146.5
1137.9      1129.2      1120.3      1111.3      1102.0      1092.6
1082.9      1073.0      1062.8      1052.4      1041.7      1030.7
1019.4      1007.7      995.6      983.1      970.0      956.5
942.3      927.4      886.2      836.9      771.6      646.7
513.3 ];
    Pressure_134a = [ 0.29269      0.31450      0.33755
0.36186      0.38749      0.41449      0.44289      0.47276      0.50413
0.53706      0.57159      0.60777      0.65466      0.68531      0.72676
0.77008      0.81530      0.86250      0.91172      0.96301      1.0165
1.0721      1.1300      1.1901      1.2527      1.3177      1.3852
1.4553      1.5280      1.6033      1.6815      1.7625      1.8464
1.9334      2.0234      2.1165      2.2130      2.3127      2.4159
2.5227      2.6331      2.9259      3.2445      3.5916      3.9721
4.0560 ];
    Volume_134a_gas = [ 0.06935      0.06470      0.06042
0.05648      0.05284      0.04948      0.04636      0.04348      0.04081
0.03833      0.03606      0.03388      0.03189      0.03003      0.02829
0.02667      0.02516      0.02374      0.02241      0.02116      0.01999
0.01890      0.01786      0.01689      0.01598      0.01511      0.01430
0.0353      0.01280      0.01212      0.01146      0.01085      0.01026

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0.00970    0.00917    0.00867    0.00818    0.00772    0.00728
0.00686    0.00646    0.00550    0.00461    0.00374    0.00265
0.00195 ];
  Enthalpy_134a_Liquid = [ 200.00    202.68    205.37
208.08    210.80    213.53    216.27    219.03    221.80
224.59    227.40    230.21    233.05    235.90    238.77
241.65    244.55    247.47    250.41    253.37    256.35
259.35    262.38    265.42    268.49    271.59    274.71
277.86    281.04    284.25    287.49    290.77    294.08
297.44    300.84    304.29    307.79    311.34    314.96
318.65    322.41    322.27    343.01    355.43    347.02
389.78 ];
  Enthalpy_134a_gas = [ 398.68    399.84    401.00
402.14    403.27    404.40    405.51    406.61    407.70
408.78    409.84    410.89    411.93    412.95    413.95
414.94    415.90    416.85    417.78    418.69    419.85
420.35    421.28    422.09    422.88    423.63    424.35
425.03    425.68    426.29    426.86    427.37    427.84
428.25    428.61    428.89    429.10    429.23    429.27
429.20    429.02    427.91    425.48    420.60    407.08
389.78 ];
  Thermal_cond_134a = [ 93.4    92.5    91.6    90.7
89.7    88.8    87.9    87    86    85.1
84.2    83.3    82.4    81.4    80.5    79.6
78.7    77.7    76.8    75.9    75    74.1
73.1    72.2    71.3    70.4    69.5    68.5
67.6    66.7    65.8    64.9    63.9    63
62.1    61.2    60.3    59.3    58.4    57.5
56.6    54.3    0    0    0    0 ];
  Viscosity_134a = [ 287.4    280.4    273.6    267.0
260.6    254.3    248.3    242.5    236.8    231.2
225.8    220.5    215.4    210.4    205.5    200.7
196.0    191.4    186.9    182.5    178.2    174.0
169.8    165.7    161.7    157.7    153.8    149.9
146.1    142.3    138.6    134.9    131.2    127.5
123.9    120.3    116.7    113.1    109.4    105.8
102.1    92.7    82.6    70.9    53.0    0 ];
  Specific_134a_Liquid = [ 1.335    1.341    1.347    1.353
1.360    1.367    1.374    1.381    1.388    1.396
1.404    1.412    1.420    1.429    1.438    1.447
1.457    1.467    1.478    1.489    1.500    1.513
1.525    1.539    1.553    1.569    1.585    1.602
1.621    1.641    1.663    1.686    1.712    1.740
1.772    1.806    1.846    1.890    1.941    2.000
2.069    2.313    2.766    3.961    0    0 ];
  Pr_134a = [ 4.108    4.065    4.023    3.983
3.951    3.915    3.881    3.849    3.822    3.793
3.765    3.738    3.712    3.694    3.671    3.648
3.629    3.614    3.597    3.580    3.564    3.553
3.542    3.532    3.522    3.515    3.508    3.506
3.503    3.501    3.503    3.504    3.515    3.521
3.535    3.550    3.573    3.605    3.636    3.680
3.732    3.949    0    0    0    0 ];
  Rho_134a_L = interp1 (T_134a, Rho_134a_Liquid, Tav_syphon);

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    Pressure      = interp1 (T_134a, Pressure_134a, Tav_syphon)*10^6;
    Volume_gas    = interp1 (T_134a, Volume_134a_gas, Tav_syphon);
    Enthalpy_134a_g= interp1 (T_134a, Enthalpy_134a_gas,
Tav_syphon)*10^3;
    Enthalpy_134a_L= interp1 (T_134a, Enthalpy_134a_Liquid,
Tav_syphon)*10^3;
    Thermal_134a  = interp1 (T_134a, Thermal_cond_134a,
Tav_syphon)*10^-3;
    Viscosity     = interp1 (T_134a, Viscosity_134a, Tav_syphon)*10^-
6;
    cp_134a      = interp1 (T_134a, Specific_134a_Liquid,
Tav_syphon)*10^3;
    Pr           = interp1 (T_134a, Pr_134a, Tav_syphon);
    Rho_134a_gas = (1 / Volume_gas);
    Kinematic    = (Viscosity / Rho_134a_L);
    Volume_134a_Liquid = (1 / Rho_134a_L);
    Enthalpy_Diff = Enthalpy_134a_g - Enthalpy_134a_L;
% rho_134a(kg/m^3), volume_gas(m^3/kg), Enthalpy_Diff(J/kg),
Pressure(Pa), Thermal_134a(W/m-K), Viscosity(Pa-s), cp_134a(J/kg-K)
    Pa = 0.10132*10^6;

Free2=(Enthalpy_Diff*(Thermal_134a^3)*(Rho_134a_L^2))/Viscosity)^0.25;
Free3=28.079*((Pressure / Pa)^0.23);
F = 0.7;
%ln(d_out/d_in)=ln(dia
%ln(0.0222/0.0212)=0.05266
ln_dia=0.05266;
Z_2=ln_dia/(2*pi*L_e*k_cu);
Z_8=ln_dia/(2*pi*L_c*k_cu);
Z_3f = (0.235*(Q_TS_1_new^(1/3))) /
((d_in^(4/3))*(G^(1/3))*L_e*(Free2^(4/3)));
Z_3p = 1/((Free3)*(G^0.2)*(Q_TS_1_new^0.4)*((pi*d_in*L_e)^0.6));
if Z_3p < Z_3f
    Z_3 = Z_3p;
else
    Z_3 = (Z_3p*F) + (Z_3f*(1 - F));
end
% Calculate Z_7
Re = (4*Q_TS_1_new)/(Enthalpy_Diff*Viscosity*pi*d_in);
if Re>1300
    Z_7 = (0.235*(Q_TS_1_new^(1/3))) /
((d_in^(4/3))*(G^(1/3))*L_c*(Free2^(4/3)))*(191*(Re^-0.733));
else
    Z_7 = (0.235*(Q_TS_1_new^(1/3))) /
((d_in^(4/3))*(G^(1/3))*L_c*(Free2^(4/3)));
end
% Calculate Z_10
a_across = (pi*((d_out^2)-(d_in^2))) / 4;
Z_10 = ((0.5*L_e) + L_a + (0.5*L_c)) / (a_across*k_cu) ;
Z_p = Z_10 / (Z_2 + Z_3 + Z_7 + Z_8);
if Z_p > 20
    Z_tot = Z_2 + Z_3 + Z_7 + Z_8;
else
    Z_tot = ((Z_2 + Z_3 + Z_7 + Z_8)^-1 + (1/Z_10))^-1;

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end
Q_TS_2_new=(Tabs_K-T_cond_new)/Z_tot;
if Q_TS_2_new <= 0
    pa2=9;
    Q_TS_1_new = Q_TS_1;
else
    pa2=abs(Q_TS_1_new-Q_TS_2_new);
    T_cond=T_cond_new;
end
end
end
!calculate QG_1
!Using DIT Global Radiation Eq.
transmissivity=0.79;
absorbitivity=0.97;
QG_1=transmissivity*absorbitivity*I*A;
!calculate QG_2
QG_2=(Q_TS_1_new*N)+Q_loss_1;
pa4=abs(QG_1-QG_2);
TG_new=TG;
end

!water
D_out=0.483726;
D_in=0.478726;
L_c= 0.478726;
K_fiber=0.036;
h_air=25;
r_tank_out=D_out/2;
r_tank_in=D_in/2;
Thermal_Al=237;
Thickness_tank=0.0015;
Thickness_insulate=0.05;
r_insulate=(L_c/2)+Thickness_tank+Thickness_insulate;
!water in tank is 100 liter
A_insulate=2*pi*r_insulate*W;
Tav_tank=(T_cond+T_water)/2;
T_water_tank = [ 273.15      275      280      285
290      295      300      305      310      315
320      325      330      335      340      345
350      355      360      365      370      373.15
375      380      385      390      400      410
420      430      440      450      460      470
480      490      500      510      520      530
540      550      560      570      580      590
600      610      620      625      630      635
640      645      647.3 ];
Specific_Volume_Liquid = [ 1.000      1.000      1.000      1.000
1.001      1.002      1.003      1.005      1.007      1.009
1.011      1.013      1.016      1.018      1.021      1.024
1.027      1.030      1.034      1.038      1.041      1.044
1.045      1.049      1.053      1.058      1.067      1.077
1.088      1.099      1.110      1.123      1.137      1.152

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1.167      1.184      1.203      1.222      1.244      1.268
1.294      1.323      1.355      1.392      1.433      1.482
1.541      1.612      1.705      1.778      1.856      1.935
2.075      2.351      3.170    ];
Specific_Heat_Liquid = [ 4.217      4.211      4.198      4.189
4.184      4.181      4.179      4.178      4.178      4.179
4.180      4.182      4.184      4.186      4.188      4.191
4.195      4.199      4.203      4.209      4.214      4.217
4.220      4.226      4.232      4.239      4.256      4.278
4.302      4.331      4.360      4.400      4.440      4.480
4.530      4.590      4.660      4.740      4.840      4.950
5.080      5.240      5.430      5.680      6.000      6.410
7.000      7.850      9.350      10.600     12.600     16.400
26.000     90.000      0.000    ];
Specific_Volume_L = interp1 (T_water_tank, Specific_Volume_Liquid,
Tav_tank)*10^-3;
Specific_Heat      = interp1 (T_water_tank, Specific_Heat_Liquid,
Tav_tank)*10^3;
Rho_water          = (1 / Specific_Volume_L);
Kinematic_water    = (Viscosity_water / Rho_water);
m_water=(0.18*Rho_water);
ln(0.28803/0.241803)+0.177581
ln=0.177581;
Z_loss=(1/(h_air*A_insulate)+(ln/(2*pi*W*K_fiber)));
Q_loss=(Tam_K-T_water)/Z_loss;
Q_st=(Q_TS_1_new*N)-Q_loss;
T_water_new=((Q_st*1800)/(Specific_Heat*m_water))+T_water;

T_w=T_water_new-273.15;
Tabs=Tabs_K-273.15;
T_c=T_cond-273.15;

fprintf('T_cond = %.3f\n',T_cond);
fprintf('T_water= %.3f\n',T_water);
fprintf('Tam= %.3f\n',Tam);
fprintf('Tam_K = %.3f\n',Tam_K);
fprintf('TG = %.3f\n',TG);
fprintf('Tabs_K = %.3f\n',Tabs_K);
fprintf('Q_loss_1 = %.3f\n',Q_loss_1);
fprintf('Q_loss_2 = %.3f\n',Q_loss_2_new);
fprintf('Q_TS_1_new = %.3f\n',Q_TS_1_new);
fprintf('Q_TS_2_new = %.3f\n',Q_TS_2_new);
fprintf('QG_1 = %.3f\n',QG_1);
fprintf('QG_2 = %.3f\n',QG_2);
fprintf('TG_new = %.3f\n',TG);
fprintf('T_cond = %.3f\n',T_cond);
fprintf('T_water_new = %.3f\n',T_water_new);
fprintf('Q_st = %.3f\n',Q_st);
fprintf('Tabs = %.3f\n',Tabs);
fprintf('T_c = %.3f\n',T_c);
fprintf('T_w = %.3f\n',T_w);
fprintf('num = %.3f\n',num);

```



ภาคผนวก ข.

ตารางสมบัติของสาร

มหาวิทยาลัยพระนคร

ตารางที่ ข.1 แสดงค่าคุณสมบัติของอากาศ [12]

TABLE A.4 Thermophysical Properties
of Gases at Atmospheric Pressure^a

T (K)	ρ (kg/m ³)	c_p (kJ/kg · K)	$\mu \cdot 10^7$ (N · s/m ²)	$\nu \cdot 10^6$ (m ² /s)	$k \cdot 10^3$ (W/m · K)	$\alpha \cdot 10^6$ (m ² /s)	Pr
Air							
100	3.5562	1.032	71.1	2.00	9.34	2.54	0.786
150	2.3364	1.012	103.4	4.426	13.8	5.84	0.758
200	1.7458	1.007	132.5	7.590	18.1	10.3	0.737
250	1.3947	1.006	159.6	11.44	22.3	15.9	0.720
300	1.1614	1.007	184.6	15.89	26.3	22.5	0.707
350	0.9950	1.009	208.2	20.92	30.0	29.9	0.700
400	0.8711	1.014	230.1	26.41	33.8	38.3	0.690
450	0.7740	1.021	250.7	32.39	37.3	47.2	0.686
500	0.6964	1.030	270.1	38.79	40.7	56.7	0.684
550	0.6329	1.040	288.4	45.57	43.9	66.7	0.683
600	0.5804	1.051	305.8	52.69	46.9	76.9	0.685
650	0.5356	1.063	322.5	60.21	49.7	87.3	0.690
700	0.4975	1.075	338.8	68.10	52.4	98.0	0.695
750	0.4643	1.087	354.6	76.37	54.9	109	0.702
800	0.4354	1.099	369.8	84.93	57.3	120	0.709
850	0.4097	1.110	384.3	93.80	59.6	131	0.716
900	0.3868	1.121	398.1	102.9	62.0	143	0.720
950	0.3666	1.131	411.3	112.2	64.3	155	0.723
1000	0.3482	1.141	424.4	121.9	66.7	168	0.726
1100	0.3166	1.159	449.0	141.8	71.5	195	0.728
1200	0.2902	1.175	473.0	162.9	76.3	224	0.728
1300	0.2679	1.189	496.0	185.1	82	238	0.719
1400	0.2488	1.207	530	213	91	303	0.703
1500	0.2322	1.230	557	240	100	350	0.685
1600	0.2177	1.248	584	268	106	390	0.688
1700	0.2049	1.267	611	298	113	435	0.685
1800	0.1935	1.286	637	329	120	482	0.683
1900	0.1833	1.307	663	362	128	534	0.677
2000	0.1741	1.337	689	396	137	589	0.672
2100	0.1658	1.372	715	431	147	646	0.667
2200	0.1582	1.417	740	468	160	714	0.655
2300	0.1513	1.478	766	506	175	783	0.647
2400	0.1448	1.558	792	547	196	869	0.630
2500	0.1389	1.665	818	589	222	960	0.613
3000	0.1135	2.726	955	841	486	1570	0.536

ตารางที่ ข.2 แสดงคุณสมบัติ น้ำอัมตัว – ตารางอุณหภูมิ [12]

TABLE A-4

Saturated water—Temperature table

Temp., T °C	Sat. press., P_{sat} kPa	Specific volume, m^3/kg		Internal energy, kJ/kg			Enthalpy, kJ/kg			Entropy, kJ/kg · K		
		Sat. liquid, v_f	Sat. vapor, v_g	Sat. liquid, u_f	Evap., u_{fg}	Sat. vapor, u_g	Sat. liquid, h_f	Evap., h_{fg}	Sat. vapor, h_g	Sat. liquid, s_f	Evap., s_{fg}	Sat. vapor, s_g
0.01	0.6117	0.001000	206.00	0.000	2374.9	2374.9	0.001	2500.9	2500.9	0.0000	9.1556	9.1556
5	0.8725	0.001000	147.03	21.019	2360.8	2381.8	21.020	2489.1	2510.1	0.0763	8.9487	9.0249
10	1.2281	0.001000	106.32	42.020	2346.6	2388.7	42.022	2477.2	2519.2	0.1511	8.7488	8.8999
15	1.7057	0.001001	77.885	62.980	2332.5	2395.5	62.982	2465.4	2528.3	0.2245	8.5559	8.7803
20	2.3392	0.001002	57.762	83.913	2318.4	2402.3	83.915	2453.5	2537.4	0.2965	8.3696	8.6661
25	3.1698	0.001003	43.340	104.83	2304.3	2409.1	104.83	2441.7	2546.5	0.3672	8.1895	8.5567
30	4.2469	0.001004	32.879	125.73	2290.2	2415.9	125.74	2429.8	2555.6	0.4368	8.0192	8.4520
35	5.6291	0.001006	25.205	146.63	2276.0	2422.7	146.64	2417.9	2564.6	0.5051	7.8466	8.3517
40	7.3851	0.001008	19.515	167.53	2261.9	2429.4	167.53	2406.0	2573.5	0.5724	7.6832	8.2556
45	9.5953	0.001010	15.251	188.43	2247.7	2436.1	188.44	2394.0	2582.4	0.6386	7.5247	8.1633
50	12.352	0.001012	12.026	209.33	2233.4	2442.7	209.34	2382.0	2591.3	0.7038	7.3710	8.0748
55	15.763	0.001015	9.5639	230.24	2219.1	2449.3	230.26	2369.8	2600.1	0.7680	7.2218	7.9898
60	19.947	0.001017	7.6670	251.16	2204.7	2455.9	251.18	2357.7	2608.8	0.8313	7.0769	7.9082
65	25.043	0.001020	6.1935	272.09	2190.3	2462.4	272.12	2345.4	2617.5	0.8937	6.9360	7.8296
70	31.202	0.001023	5.0396	293.04	2175.8	2468.9	293.07	2333.0	2626.1	0.9551	6.7989	7.7540
75	38.597	0.001026	4.1291	313.99	2161.3	2475.3	314.03	2320.6	2634.6	1.0158	6.6655	7.6812
80	47.416	0.001029	3.4053	334.97	2146.6	2481.6	335.02	2308.0	2643.0	1.0756	6.5355	7.6111
85	57.868	0.001032	2.8261	355.96	2131.9	2487.8	356.02	2295.3	2651.4	1.1346	6.4089	7.5435
90	70.183	0.001036	2.3593	376.97	2117.0	2494.0	377.04	2282.5	2659.6	1.1929	6.2853	7.4782
95	84.609	0.001040	1.9808	398.00	2102.0	2500.1	398.09	2269.6	2667.6	1.2504	6.1647	7.4151
100	101.42	0.001043	1.6720	419.06	2087.0	2506.0	419.17	2256.4	2675.6	1.3072	6.0470	7.3542
105	120.90	0.001047	1.4186	440.15	2071.8	2511.9	440.28	2243.1	2683.4	1.3634	5.9319	7.2952
110	143.38	0.001052	1.2094	461.27	2056.4	2517.7	461.42	2229.7	2691.1	1.4188	5.8193	7.2382
115	169.18	0.001056	1.0360	482.42	2040.9	2523.3	482.59	2216.0	2698.6	1.4737	5.7092	7.1829
120	198.67	0.001060	0.89133	503.60	2025.3	2528.9	503.81	2202.1	2706.0	1.5279	5.6013	7.1292
125	232.23	0.001065	0.77012	524.83	2009.5	2534.3	525.07	2188.1	2713.1	1.5816	5.4956	7.0771
130	270.28	0.001070	0.66808	546.10	1993.4	2539.5	546.38	2173.7	2720.1	1.6346	5.3919	7.0265
135	313.22	0.001075	0.58179	567.41	1977.3	2544.7	567.75	2159.1	2726.9	1.6872	5.2901	6.9773
140	361.53	0.001080	0.50850	588.77	1960.9	2549.6	589.16	2144.3	2733.5	1.7392	5.1901	6.9294
145	415.68	0.001085	0.44600	610.19	1944.2	2554.4	610.64	2129.2	2739.8	1.7908	5.0919	6.8827
150	476.16	0.001091	0.39248	631.66	1927.4	2559.1	632.18	2113.8	2745.9	1.8418	4.9953	6.8371
155	543.49	0.001096	0.34648	653.19	1910.3	2563.5	653.79	2098.0	2751.8	1.8924	4.9002	6.7927
160	618.23	0.001102	0.30680	674.79	1893.0	2567.8	675.47	2082.0	2757.5	1.9426	4.8066	6.7492
165	700.93	0.001108	0.27244	695.46	1875.4	2571.9	697.24	2065.6	2762.8	1.9923	4.7143	6.7067
170	792.18	0.001114	0.24260	718.20	1857.5	2575.7	719.08	2048.8	2767.9	2.0417	4.6233	6.6650
175	892.60	0.001121	0.21659	740.02	1839.4	2579.4	741.02	2031.7	2772.7	2.0906	4.5335	6.6242
180	1002.8	0.001127	0.19384	761.92	1820.9	2582.8	763.05	2014.2	2777.2	2.1392	4.4448	6.5841
185	1123.5	0.001134	0.17390	783.91	1802.1	2586.0	785.19	1996.2	2781.4	2.1875	4.3572	6.5447
190	1255.2	0.001141	0.15636	806.00	1783.0	2589.0	807.43	1977.9	2785.3	2.2355	4.2705	6.5059
195	1398.8	0.001149	0.14089	828.18	1763.6	2591.7	829.78	1959.0	2788.8	2.2831	4.1847	6.4678
200	1554.9	0.001157	0.12721	850.46	1743.7	2594.2	852.26	1939.8	2792.0	2.3305	4.0997	6.4302

ตารางที่ ข.2 แสดงคุณสมบัติ น้ำอิมตัว – ตารางอุณหภูมิ (ต่อ)

TABLE A-4

Saturated water—Temperature table (Continued)

Temp., T °C	Sat. press., P_{sat} kPa	Specific volume, m^3/kg		Internal energy, kJ/kg			Enthalpy, kJ/kg			Entropy, $kJ/kg \cdot K$		
		Sat. liquid, v_f	Sat. vapor, v_g	Sat. liquid, u_f	Evap., u_{fg}	Sat. vapor, u_g	Sat. liquid, h_f	Evap., h_{fg}	Sat. vapor, h_g	Sat. liquid, s_f	Evap., s_{fg}	Sat. vapor, s_g
205	1724.3	0.001164	0.11508	872.86	1723.5	2596.4	874.87	1920.0	2794.8	2.3776	4.0154	6.3930
210	1907.7	0.001173	0.10429	895.38	1702.9	2598.3	897.61	1899.7	2797.3	2.4245	3.9318	6.3563
215	2105.9	0.001181	0.094680	918.02	1681.9	2599.9	920.50	1878.8	2799.3	2.4712	3.8489	6.3200
220	2319.6	0.001190	0.086094	940.79	1660.5	2601.3	943.55	1857.4	2801.0	2.5176	3.7664	6.2840
225	2549.7	0.001199	0.078405	963.70	1638.6	2602.3	966.76	1835.4	2802.2	2.5639	3.6844	6.2483
230	2797.1	0.001209	0.071505	986.76	1616.1	2602.9	990.14	1812.8	2802.9	2.6100	3.6028	6.2128
235	3062.6	0.001219	0.065300	1010.0	1593.2	2603.2	1013.7	1789.5	2803.2	2.6560	3.5216	6.1776
240	3347.0	0.001229	0.059707	1033.4	1569.8	2603.1	1037.5	1765.5	2803.0	2.7018	3.4405	6.1424
245	3651.2	0.001240	0.054656	1056.9	1545.7	2602.7	1061.5	1740.8	2802.2	2.7476	3.3596	6.1072
250	3976.2	0.001252	0.050085	1080.7	1521.1	2601.8	1085.7	1715.3	2801.0	2.7933	3.2788	6.0721
255	4322.9	0.001263	0.045941	1104.7	1495.8	2600.5	1110.1	1689.0	2799.1	2.8390	3.1979	6.0369
260	4692.3	0.001276	0.042175	1128.8	1469.9	2598.7	1134.8	1661.8	2796.6	2.8847	3.1169	6.0017
265	5085.3	0.001289	0.038748	1153.3	1443.2	2596.5	1159.8	1633.7	2793.5	2.9304	3.0358	5.9662
270	5503.0	0.001303	0.035622	1177.9	1415.7	2593.7	1185.1	1604.6	2789.7	2.9762	2.9542	5.9305
275	5946.4	0.001317	0.032767	1202.9	1387.4	2590.3	1210.7	1574.5	2785.2	3.0221	2.8723	5.8944
280	6416.6	0.001333	0.030153	1228.2	1358.2	2586.4	1236.7	1543.2	2779.9	3.0681	2.7898	5.8579
285	6914.6	0.001349	0.027756	1263.7	1328.1	2581.8	1263.1	1510.7	2773.7	3.1144	2.7066	5.8210
290	7441.8	0.001366	0.025554	1279.7	1296.9	2576.5	1289.8	1476.9	2766.7	3.1608	2.6225	5.7834
295	7999.0	0.001384	0.023528	1306.0	1264.5	2570.5	1317.1	1441.6	2758.7	3.2076	2.5374	5.7450
300	8587.9	0.001404	0.021659	1332.7	1230.9	2563.6	1344.8	1404.8	2749.6	3.2548	2.4511	5.7059
305	9209.4	0.001425	0.019932	1360.0	1195.9	2555.8	1373.1	1366.3	2739.4	3.3024	2.3633	5.6657
310	9865.0	0.001447	0.018333	1387.7	1159.3	2547.1	1402.0	1325.9	2727.9	3.3506	2.2737	5.6243
315	10,556	0.001472	0.016849	1416.1	1121.1	2537.2	1431.6	1283.4	2715.0	3.3994	2.1821	5.5816
320	11,284	0.001499	0.015470	1445.1	1080.9	2526.0	1462.0	1238.5	2700.6	3.4491	2.0881	5.5372
325	12,051	0.001528	0.014183	1475.0	1038.5	2513.4	1493.4	1191.0	2684.3	3.4998	1.9911	5.4908
330	12,858	0.001560	0.012979	1505.7	993.5	2499.2	1525.8	1140.3	2666.0	3.5516	1.8906	5.4422
335	13,707	0.001597	0.011848	1537.5	945.5	2483.0	1559.4	1086.0	2645.4	3.6050	1.7857	5.3907
340	14,601	0.001638	0.010783	1570.7	893.8	2464.5	1594.6	1027.4	2622.0	3.6602	1.6756	5.3358
345	15,541	0.001685	0.009772	1605.5	837.7	2443.2	1631.7	963.4	2595.1	3.7179	1.5585	5.2765
350	16,529	0.001741	0.008806	1642.4	775.9	2418.3	1671.2	892.7	2563.9	3.7788	1.4326	5.2114
355	17,570	0.001808	0.007872	1682.2	706.4	2388.6	1714.0	812.9	2526.9	3.8442	1.2942	5.1384
360	18,666	0.001885	0.006950	1726.2	625.7	2351.9	1761.5	720.1	2481.6	3.9165	1.1373	5.0537
365	19,822	0.002015	0.006009	1777.2	526.4	2303.6	1817.2	605.5	2422.7	4.0004	0.9489	4.9493
370	21,044	0.002217	0.004953	1844.5	385.6	2230.1	1891.2	443.1	2334.3	4.1119	0.6890	4.8009
373.95	22,064	0.003106	0.003106	2015.7	0	2015.7	2084.3	0	2084.3	4.4070	0	4.4070

TABLE A.6 Thermophysical Properties of Saturated Water^a

Temperature, T (K)	Pressure, P (bars)		Specific Volume (m ³ /kg)		h_f (kJ/kg)	Heat of Vaporization, h_{fg} (kJ/kg)		Specific Heat (kJ/kg · K)		Viscosity (N · s/m ²)		Thermal Conductivity (W/m · K)		Prandtl Number		Surface Tension, $\sigma_f \cdot 10^3$ (N/m)	Expansion Coefficient, $\beta_f \cdot 10^6$ (K ⁻¹)	Temperature, T (K)
	$\rho_f \cdot 10^3$	ρ_g	v_f	v_g		$c_{p,f}$	$c_{p,g}$	$\mu_f \cdot 10^6$	$\mu_g \cdot 10^6$	$k_f \cdot 10^3$	$k_g \cdot 10^3$	Pr_f	Pr_g					
273.15	0.00511	1.000	206.3	2502	4.217	1.854	1750	8.02	569	18.2	12.99	0.815	75.5	-68.05	273.15			
275	0.00597	1.000	181.7	2497	4.211	1.855	1652	8.09	574	18.3	12.22	0.817	75.3	-32.74	275			
280	0.00990	1.000	130.4	2485	4.198	1.858	1422	8.29	582	18.6	10.26	0.825	74.8	46.04	280			
285	0.01387	1.000	99.4	2473	4.189	1.861	1225	8.49	590	18.9	8.81	0.833	74.3	114.1	285			
290	0.01917	1.001	69.7	2461	4.184	1.864	1080	8.69	598	19.3	7.56	0.841	73.7	174.0	290			
295	0.02617	1.002	51.94	2449	4.181	1.868	959	8.89	606	19.5	6.62	0.849	72.7	227.5	295			
300	0.03531	1.003	39.13	2438	4.179	1.872	855	9.09	613	19.6	5.83	0.857	71.7	276.1	300			
305	0.04712	1.005	29.74	2426	4.178	1.877	769	9.29	620	20.1	5.20	0.865	70.9	320.6	305			
310	0.06221	1.007	22.93	2414	4.178	1.882	695	9.49	628	20.4	4.62	0.873	70.0	361.9	310			
315	0.08132	1.009	17.82	2402	4.179	1.888	631	9.69	634	20.7	4.16	0.883	69.2	400.4	315			
320	0.1053	1.011	13.98	2390	4.180	1.895	577	9.89	640	21.0	3.77	0.894	68.3	436.7	320			
325	0.1351	1.013	11.06	2378	4.182	1.903	528	10.09	645	21.3	3.42	0.901	67.5	471.2	325			
330	0.1719	1.016	8.82	2366	4.184	1.911	489	10.29	650	21.7	3.15	0.908	66.6	504.0	330			
335	0.2167	1.018	7.09	2354	4.186	1.920	453	10.49	656	22.0	2.88	0.916	65.8	535.5	335			
340	0.2713	1.021	5.74	2342	4.188	1.930	420	10.69	660	22.3	2.66	0.925	64.9	566.0	340			
345	0.3372	1.024	4.683	2329	4.191	1.941	389	10.89	668	22.6	2.45	0.933	64.1	595.4	345			
350	0.4163	1.027	3.846	2317	4.195	1.954	365	11.09	668	23.0	2.29	0.942	63.2	624.2	350			
355	0.5100	1.030	3.180	2304	4.199	1.968	343	11.29	671	23.3	2.14	0.951	62.3	652.3	355			
360	0.6209	1.034	2.645	2291	4.203	1.983	324	11.49	674	23.7	2.02	0.960	61.4	697.9	360			
365	0.7514	1.038	2.212	2278	4.209	1.999	306	11.69	677	24.1	1.91	0.969	60.5	707.1	365			
370	0.9040	1.041	1.861	2265	4.214	2.017	289	11.89	679	24.5	1.80	0.978	59.5	728.7	370			
373.15	1.0133	1.044	1.679	2257	4.217	2.029	279	12.02	680	24.8	1.76	0.984	58.9	750.1	373.15			
375	1.0815	1.045	1.574	2252	4.220	2.036	274	12.09	681	24.9	1.70	0.987	58.6	761	375			
380	1.2869	1.049	1.337	2239	4.226	2.057	260	12.29	683	25.4	1.61	0.999	57.6	788	380			
385	1.5233	1.053	1.142	2225	4.232	2.080	248	12.49	685	25.8	1.53	1.004	56.6	814	385			

ตารางที่ ข.3 แสดงค่าคุณสมบัติของน้ำ [12]

ตารางที่ ข.4 แสดงค่าคุณสมบัติของสารทำงาน R-134a [12]

Temp °C	Pressure MPa	Density kg/m ³		Volume m ³ /kg		Enthalpy kJ/kg		Entropy kJ/(kg.K)		Specific Heat kJ/(kg.K)		Viscosity μPas		Thermal Cond mW/(m.K)		Surface Tension mN/m
		Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	
-26.07b	0.10132	1374.3	0.19016	166.07	382.90	0.8701	1.7476	1.268	0.784	406.4	9.79	105.4	9.52	15.54		
10.00	0.41449	1260.2	0.04948	213.53	404.40	1.0483	1.7224	1.367	0.930	254.3	11.42	88.8	12.66	10.30		
12.00	0.44289	1253.3	0.04636	216.27	405.51	1.0579	1.7215	1.374	0.939	248.3	11.52	87.9	12.84	10.02		
14.00	0.47276	1246.3	0.04348	219.03	406.61	1.0674	1.7207	1.381	0.950	242.5	11.62	87.0	13.02	9.74		
16.00	0.50413	1239.3	0.04081	221.80	407.70	1.0770	1.7199	1.388	0.960	236.8	11.72	86.0	13.20	9.47		
18.00	0.53706	1232.1	0.03833	224.59	408.78	1.0865	1.7191	1.396	0.971	231.2	11.82	85.1	13.39	9.19		
20.00	0.57159	1224.9	0.03603	227.40	409.84	1.0960	1.7183	1.404	0.982	225.8	11.92	84.2	13.57	8.92		
22.00	0.60777	1217.5	0.03388	230.21	410.89	1.1055	1.7176	1.412	0.994	220.5	12.03	83.3	13.76	8.65		
24.00	0.64566	1210.1	0.03189	233.05	411.93	1.1149	1.7169	1.420	1.006	215.4	12.14	82.4	13.96	8.38		
26.00	0.68531	1202.6	0.03003	235.90	412.95	1.1244	1.7162	1.429	1.018	210.4	12.25	81.4	14.15	8.11		
28.00	0.72676	1194.9	0.02829	238.77	413.95	1.1338	1.7155	1.438	1.031	205.5	12.36	80.5	14.35	7.84		
30.00	0.77008	1187.2	0.02667	241.65	414.94	1.1432	1.7149	1.447	1.044	200.7	12.48	79.6	14.56	7.57		
32.00	0.81530	1179.3	0.02516	244.55	415.90	1.1527	1.7142	1.457	1.058	196.0	12.60	78.7	14.76	7.31		
34.00	0.86250	1171.3	0.02374	247.47	416.85	1.1621	1.7135	1.467	1.073	191.4	12.72	77.7	14.97	7.05		

Refrigerant 134a Properties of Saturated Liquid and Saturated Vapor

ตารางที่ ข.4 แสดงค่าคุณสมบัติของสารทำงาน R-134a (ต่อ)

Temp °C	Pressure MPa	Density kg/m ³		Volume m ³ /kg		Enthalpy kJ/kg		Entropy kJ/(kg.K)		Specific Heat kJ/(kg.K)		Viscosity μ Pas		Thermal Cond mW/(m.K)		Surface Tension mN/m
		Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	
36.00	0.91172	1163.2	0.02241	250.41	417.78	1.1715	1.7129	1.478	1.088	186.9	12.84	72.9	15.19	6.78		
38.00	0.96301	1154.9	0.02116	253.37	418.69	1.1809	1.7122	1.489	1.104	182.5	12.97	75.9	15.41	6.52		
40.00	1.0165	1146.5	0.01999	256.35	419.58	1.1903	1.7115	1.500	1.120	178.2	13.10	75.0	15.64	6.27		
42.00	1.0721	1137.9	0.01890	259.35	420.44	1.1997	1.7108	1.513	1.138	174.0	13.24	74.1	15.86	6.01		
44.00	1.1300	1129.2	0.01786	262.38	421.28	1.2091	1.7101	1.525	1.156	169.8	13.38	73.1	16.10	5.76		
46.00	1.1901	1120.3	0.01689	265.42	422.09	1.2185	1.7094	1.539	1.175	165.7	13.52	72.2	16.34	5.51		
48.00	1.2527	1111.3	0.0159	268.49	422.88	1.2279	1.7086	1.553	1.196	161.7	13.67	71.3	16.59	5.26		
50.00	1.3177	1102.0	0.01511	271.59	423.63	1.2373	1.7078	1.569	1.218	157.7	13.83	70.4	16.84	5.01		
52.00	1.3852	1092.6	0.01430	274.71	424.35	1.2468	1.7070	1.585	1.241	153.8	13.99	69.5	17.10	4.76		
54.00	1.4553	1082.9	0.01353	277.86	425.03	1.2562	1.7061	1.602	1.266	149.9	14.16	68.5	17.36	4.52		
56.00	1.5280	1073.0	0.01280	281.04	425.68	1.2657	1.7051	1.621	1.293	146.1	14.33	67.6	17.63	4.28		
58.00	1.6033	1062.8	0.01212	284.25	426.29	1.2752	1.7041	1.641	1.322	142.3	14.51	66.7	17.91	4.04		
60.00	1.6815	1052.4	0.01146	287.49	426.86	1.2847	1.7031	1.663	1.354	138.6	14.71	65.8	18.19	3.81		
62.00	1.7625	1041.7	0.01085	290.77	427.37	1.2943	1.7019	1.686	1.388	134.9	14.91	64.9	18.48	3.57		

ตารางที่ ข.4 แสดงค่าคุณสมบัติของสารทำงาน R-134a (ต่อ)

Temp °C	Pressure MPa	Density kg/m ³		Volume m ³ /kg		Enthalpy kJ/kg		Entropy kJ/(kg.K)		Specific Heat kJ/(kg.K)		Viscosity μ Pa.s		Thermal Cond mW/(m.K)		Surface Tension mN/m
		Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	
64.00	1.8464	1030.7	0.01026	294.08	427.84	1.3039	1.7007	1.712	1.426	131.2	15.12	63.9	18.78	3.34		
66.00	1.9334	1019.4	0.00970	297.44	428.25	1.3136	1.6993	1.740	1.468	127.5	15.35	63.0	19.09	3.12		
68.00	2.0234	1007.7	0.00917	300.84	428.61	1.3234	1.6979	1.772	1.515	123.9	15.59	62.1	19.40	2.89		
70.00	2.1165	995.6	0.00867	304.29	428.89	1.3332	1.6963	1.806	1.567	120.3	15.85	61.2	19.72	2.67		
72.00	2.2130	983.1	0.00818	307.79	429.10	1.3430	1.6945	1.846	1.642	116.7	16.12	60.3	20.05	2.46		
74.00	2.3127	970.0	0.00772	311.34	429.23	1.3530	1.6926	1.890	1.693	113.1	16.41	59.3	20.39	2.24		
76.00	2.4159	956.5	0.00728	314.96	429.27	1.3631	1.6905	1.941	1.770	109.4	16.73	58.4	20.74	2.03		
78.00	2.5277	942.3	0.00686	318.65	429.20	1.3733	1.6881	2.000	1.861	105.8	17.08	57.5	21.09	1.83		
80.00	2.6331	927.4	0.00646	322.41	429.02	1.3837	1.6855	2.069	1.967	102.1	17.46	56.6	21.46	1.63		
85.00	2.9259	886.2	0.00550	332.27	427.91	1.4105	1.6775	2.313	2.348	92.7	18.59	54.3	22.41	1.15		
90.00	3.2445	836.9	0.00461	343.01	425.48	1.4392	1.6663	2.766	3.064	82.6	20.15	-	-	0.72		
95.00	3.5916	771.6	0.00374	355.434	420.60	1.4720	1.6490	3.961	4.942	70.9	22.59	-	-	0.33		
100.00	3.9721	646.7	0.00265	374.02	407.08	1.5207	1.6093	-	-	53.0	28.86	-	-	0.03		

b= boiling point



ภาคผนวก ค.

อื่นๆ

มหาวิทยาลัยนเรศวร

ตารางที่ ค.1 ค่าพลังงานแสงอาทิตย์และอุณหภูมิอากาศของจังหวัดพิษณุโลก จากกรมอุตุนิยมวิทยา

วัน/เดือน/ปี	เวลา	Global Radiation (W/m ²)	Ambient Temperature (°C)
2/4/2008	6:00:00	8.2905	25.75
2/4/2008	6:30:00	46.0010	27.03
2/4/2008	7:00:00	116.8416	28.25
2/4/2008	7:30:00	204.0354	29.45
2/4/2008	8:00:00	291.0552	30.51
2/4/2008	8:30:00	371.8354	31.56
2/4/2008	9:00:00	466.5760	32.10
2/4/2008	9:30:00	535.4864	34.10
2/4/2008	10:00:00	589.2604	35.21
2/4/2008	10:30:00	679.1093	36.15
2/4/2008	11:00:00	761.5895	37.08
2/4/2008	11:30:00	812.1489	38.08
2/4/2008	12:00:00	840.8229	38.95
2/4/2008	12:30:00	845.1770	39.15
2/4/2008	13:00:00	817.9072	38.81
2/4/2008	13:30:00	772.8010	38.15
2/4/2008	14:00:00	721.5239	37.23
2/4/2008	14:30:00	658.9125	36.33
2/4/2008	15:00:00	593.3000	35.43
2/4/2008	15:30:00	484.1343	34.60
2/4/2008	16:00:00	348.8260	33.73
2/4/2008	16:30:00	251.6479	32.68
2/4/2008	17:00:00	161.4208	31.68
2/4/2008	17:30:00	76.1000	30.78
2/4/2008	18:00:00	24.5	29.58
2/4/2008	18:30:00	0	28.78

ตารางที่ ค.2 แสดงราคาท่อทองแดงชนิดเส้นตรง [11]

TYPE M (ASTM-B88) ความยาว 6 เมตร

SIZE (OD)	WALL THICKNESS	LIST PRICE
3/8"	0.022"	400
1/2"	0.025"	570
5/8"	0.028"	830
3/4"	0.030"	1,085
7/8"	0.032"	1,315
1-1/8"	0.035"	1,885
1-3/8"	0.042"	3,485
1-5/8"	0.050"	4,800
2-1/8"	0.060"	7,485
2-5/8"	0.070"	10,920
3-1/8"	0.080"	14,400

TYPE L (ASTM-B88) ความยาว 6 เมตร

SIZE(OD)	WALL THICKNESS	LIST PRICE
3/8"	0.030"	630
1/2"	0.035"	1,000
5/8"	0.040"	1,435
3/4"	0.042"	1,770
7/8"	0.045"	2,315
1-1/8"	0.050"	3,200
1-3/8"	0.055"	4,515
1-5/8"	0.060"	5,770
2-1/8"	0.070"	8,630
2-5/8"	0.080"	13,080
3-1/8"	0.090"	17,160

ตารางที่ ก.2 แสดงราคาท่อทองแดงชนิดเส้นตรง (ต่อ)

TYPE K (ASTM-B88) ความยาว 6 เมตร

SIZE(OD)	WALL THICKNESS	LIST PRICE
3/8"	0.035"	920
1/2"	0.049"	1,560
5/8"	0.049"	1,910
3/4"	0.049"	2,830
7/8"	0.065"	3,530
1-1/8"	0.065"	4,670
1-3/8"	0.065"	6,355
1-5/8"	0.072"	8,150
2-1/8"	0.083"	12,240
2-5/8"	0.095"	20,085
3-1/8"	0.109"	29,460